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Computational Study of Mixed Convection Flow with Algebraic Decay of Mainstream Velocity in the Presence of Applied Magnetic Field

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Abstract

The present study concern with the two dimensional viscous, incompressible, electrically con ducting, mixed convection flows with algebraic decay of mainstream velocity $U(x)=(1-x)^a$. The physical phenomenon of the problem is simulated by using the Primitive Variable Formulation (PVF) for Finite Difference Method (FDM) and Stream Function Formulation (SFF) for Local Non-Similarity Method (LNS). The physical behaviors of momentum and temperature fields are given graphically. The results obtained for skin friction and rate of heat transfer for different values of physical parameters are also compared by both methods and presented in tabular form.

Keywords: Mixed convection; Heat transfer; Skin friction; Algebraic decay of mainstream velocity

Introduction

When the surface temperature is different from the ambient fluid temperature, it gives rise to a density gradient in the thermal boundary layer region. This density gradient produces a body force in the form of buoyancy of the fluid. The buoyancy force along with some external force constitutes a mixed convection flow. There the external force can either be in the form of free stream or some moving or stretching surface. With this understanding, we formulate the problem of mixed convection flow and the possible literature survey for the problem under consideration is given in preceding paragraph.

Ostrach [1] presented the similarity solution of natural convection along vertical isothermal plate. The instantaneous action of buoyancy and induced magnetic forces leading to natural convection heat transfer was investigated by Sparrow et al. [2]. They found out that in the presence of magnetic field, the natural convection heat transfer to liquid metals may be considerably affected [3]. The mixed convection over a horizontal surface due to uniform free stream has been studied by many researchers. Gebhart [4] used an analytical technique to analyze the effect of dissipation on natural convection [5,6]. The joint free and forced convection along with uniform heat flux in the presence of strong magnetic field was studied by Lioyd el al. [7]. Dwivedi [8] examined the free convection oscillatory hydromagnetic laminar flow of a viscous, electrically conducting and incompressible fluid over a vertical infinite porous plate under the influence of a transverse magnetic field when the temperature or heat flux at the surface oscillates in magnitude but not in direction. Soundalgekar [9] studied natural convection flow along vertical porous plate with suction and viscous dissipation [10].

A particular self-similar solution of the mixed convection flow over a horizontal surface was presented by Schneider [11] for the case of specified wall temperature as an inverse square root of the distance from the top edge. Chakrobarti et al. [12] illustrated the heat transfer and flow of an incompressible electrically conducting fluid pass a stretching sheet. They presented an analytical solution for the flow and the numerical solution for the heat transfer. Under the influence of free stream oscillations, Perdikis et al. [13] examined the laminar free convection and mass transfer effects of a viscous, incompressible heat generating fluid-flow along an impulsively vertical plate with heat flux and constant suction at the plate. Wantanabe et al. [14] investigated the heat transfer in thermal boundary layer of MHD flow over a flat plate. The mixed convection boundary layer flow of an incompressible, viscous and electrically conducting fluid in the presence of transverse magnetic field along a vertical porous plate was examined by Hosain et al. [15]. In the presence of Hall current effect, Chamkha [16] expressed the MHD free convection pass a vertical plate in thermally satisfied porous medium. Chen [17] presented his study on MHD natural convection flow over a permeable inclined surface with variable wall temperature and concentration. He studied that increasing the angle of inclination decreases the effect of buoyancy force. Mostafa [18] studied the heat transfer and flow of an incompressible electrically conducting viscous fluid which passes a continuously moving vertical infinite plate with uniform suction and heat flux under the action of radiation taking into account the effects of variable viscosity. Considering a homogeneous chemical reaction of first order, Odat et al. [19] numerically examined the effect of magnetic field on the transient free convection flow of an electrically conducting fluid pass an impulsively started isothermal vertical plate. They observed that increasing the chemical reaction parameter decreases the velocity and concentration. Makinde [20] performed an analysis to examine the hydromagnetic mixed convection flow of a viscous, incompressible and electrically conducting fluid and mass transfer along a vertical porous plate with constant heat flux embedded in a porous medium.

However, when the free convective flows occur at high temperatures, radiation effects on the flow become significant. Many processes in engineering areas occur at high temperatures and knowledge of radiative heat transfer becomes very important for the design of the pertinent equipment. Nuclear power plants, gas turbines and the various propulsion devices for aircraft, missiles and space vehicles are examples of such engineering areas. The inclusion of radiation effects in the energy equation leads to a highly non-linear partial differential equation. Under the influence of thermal radiation along with variable

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suction and thermophoresis. Alam et al. [21] numerically examined the two-dimensional steady MHD mixed convection and mass transfer flow through an inclined semi-infinite porous plate. In the presence of transversely applied magnetic field, MHD flow of an electrically conducting, viscous and incompressible fluid through a semi-infinite vertical plate with mass transfer was examined by Palani et al. [22]. Ferdows et al. [23] presented MHD boundary layer flow of a nanofluid through an exponentially stretching sheet. They also discussed and observed the heat transfer characteristics and the effects of governing parameters on the flow field. Ashraf et al. [24] studied the mixed convection flow past a magnetized vertical porous plate numerically.

In the light of above literature survey, we formulate the problem of mixed convection flow with algebraic decay of mainstream velocity in the presence of applied magnetic field.

Mathematical Analysis and Governing Equations

In this section, we formulate the bulk of mathematical equations governing the MHD convective flow along a vertical flat plate. We combine the basic momentum and energy equations into self-consistent system. This set of equations considers steady two dimensional flow of viscous incompressible conducting fluid along a semi-infinite vertical surface. The decay is only algebraic for $0 < \alpha < 1$ (Figure 1). A magnetic field of strength Bo(x) is considered to be applied parallel to the *y*-axis which is normal to the plate. Under the usual Boussinesq approximation, the flow is governed by the following boundary layer equations following by Merkin [10].

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$u\frac{\partial u}{\partial x} + v\frac{\partial v}{\partial y} = U\frac{dU}{dx} + v\frac{\partial^2 u}{\partial y^2} + g\beta(T - T_{\infty}) - \frac{\sigma B_0^2}{\rho}u \qquad (1)$$

$$u\frac{\partial T}{\partial x} + v\frac{\partial T}{\partial y} = \alpha\frac{\partial^2 T}{\partial y^2}$$

where

$$U(x) = (1-x)^{-\alpha}$$

The appropriate boundary conditions for the present problem are



$$u(x,0) = 0, \quad v(x,0) = 0, \quad T(x,0) = T_w$$
 (2)

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$$u(\infty) = U(x), \quad T(\infty) = T_{\infty}$$

By using the dimensionless variables

$$\overline{x} = \frac{x}{L}, \quad \overline{y} = R_{ex}^{\frac{1}{2}} \frac{y}{L}, \quad \overline{u} = \frac{u}{U_0}, \quad \overline{v} = R_{ex}^{\frac{1}{2}} \frac{v}{U_0}$$
$$\overline{\theta} = \frac{\overline{T} - \overline{T}_{\infty}}{\overline{T}_w - \overline{T}_{\infty}}, \quad \overline{U} = \frac{U}{U_0}$$
(3)

The dimensionless boundary layer equations along with boundary conditions are given as:

$$\frac{\partial \overline{u}}{\partial \overline{x}} + \frac{\partial \overline{v}}{\partial \overline{y}} = 0 \tag{4}$$

$$\overline{u}\frac{\partial\overline{u}}{\partial\overline{x}} + \overline{v}\frac{\partial\overline{u}}{\partial\overline{y}} = \overline{U}\frac{d\overline{U}}{d\overline{x}} + \frac{\partial^{2}\overline{u}}{\partial\overline{y}^{2}} + \lambda\overline{\theta} - M\overline{u}$$
(5)

$$\overline{u}\frac{\partial\overline{\theta}}{\partial\overline{x}} + \overline{v}\frac{\partial\overline{\theta}}{\partial\overline{y}} = \frac{1}{P_r}\frac{\partial^2\overline{\theta}}{\partial\overline{v}^2}$$
(6)

The dimensionless boundary conditions are:

$$\overline{u}(x,0) = 0, \quad \overline{v}(x,0) = 0, \quad \overline{\theta}(x,0) = 1$$

$$\overline{u}(\infty) = \overline{U}(x) \quad \overline{\theta}(\infty) = 0$$
(7)

where

$$\lambda = \frac{G_{rL}}{R_{eL}^2}, \quad G_{rL} = \frac{g\beta\Delta TL^3}{v^2}, \quad R_{eL} = \frac{U_0L}{v}, \quad M = \frac{\sigma B_0^2 x^{-1}}{\rho U_0}, \quad P_r = \frac{v}{\alpha}$$

the Richardson Grashof number, Reynolds number, magnetic parameter, Prandtl number and the characteristic length respectively.

Method of Solutions

We now turn to get the numerical solutions of the problem. For this purpose we will use Primitive variable formulation for Finite Difference Method and Stream function formulation for Local Non-Similarity Method.

Primitive variable formulation

We now introduce the group of transformations that is known as Primitive Variable Formulation (PVF) to transform the given system of equations into convenient form for integration

$$\overline{u} = U(\xi, Y), \quad \overline{v} = \overline{x^2} V(\xi, Y), \quad \overline{U} = (1 - \overline{x})^{-\alpha}$$

$$(8)$$

$$\overline{\theta} = \overline{x}^{-1} \theta(\xi, Y), \quad Y = \overline{x}^{-2} \overline{y}, \quad \xi = -\overline{x}$$

Thus (5) and (6) becomes

$$U\xi \frac{\partial U}{\partial \xi} - \left(\frac{1}{2}YU + V\xi\right)\frac{\partial U}{\partial Y} = \frac{\partial^2 U}{\partial Y^2} + \lambda\theta - MU - \alpha\xi(1+\xi)^{-2\alpha-1}$$
(9)

$$U\xi \frac{\partial U}{\partial \xi} - \left(\frac{1}{2}YU + V\xi\right)\frac{\partial \theta}{\partial Y} - U\theta = \frac{1}{P_r}\frac{\partial^2 \theta}{\partial Y^2}$$
(10)

The appropriate boundary conditions satisfied by the above system of equations are

$$U(\xi, 0) = V(\xi, 0) = 0, \quad \theta(\xi, 0) = 1$$
(11)

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 $V(\xi,\infty) = 1, \quad \theta(\xi,\infty) = 0$

Discretization: Now we first discretize (9)-(20) using FDM (Finite Difference Method)

$$\frac{\partial U}{\partial \xi} = \frac{U_{i,j} - U_{i,j+1}}{\Delta \xi}$$

$$\frac{\partial U}{\partial Y} = \frac{U_{i+1,j} - U_{i-1,j}}{2\Delta Y}$$
(12)

$$\frac{\partial^2 U}{\partial Y^2} = \frac{U_{i+1,j} - 2U_{i,j} + U_{i-1,j}}{\Delta Y^2}$$

and get discretized form

$$A_{l}U_{i+1,j} - B_{l}U_{i,j} + C_{l}U_{i-1,j} = D_{l}$$
(13)
where

$$A_{l} = 1 + \frac{1}{2}\Delta Y \left(\frac{1}{2}Y_{j}U_{i,j} + V_{i,j}\xi_{i}\right)$$

$$B_{l} = 2 + \frac{\Delta Y^{2}}{\Delta \xi}U_{i,j}\xi_{i} + M\Delta Y^{2}$$

$$C_{l} = 1 - \frac{1}{2}\Delta Y \left(\frac{1}{2}Y_{j}U_{i,j} + V_{i,j}\xi_{i}\right)$$

$$D_{l} = -\frac{\Delta Y^{2}}{\Delta \xi}U_{i,j}\xi_{i}U_{i,j+1} - \lambda\theta_{i,j}\Delta Y^{2} + \alpha\xi_{i}(1+\xi_{i})^{-2\alpha-1}\Delta Y^{2}$$
(14)

Similarly we discretize (10) using FDM

$$\frac{\partial \theta}{\partial \xi} = \frac{\theta_{i,j} - \theta_{i,j+1}}{\Delta \xi}$$

$$\frac{\partial \theta}{\partial Y} = \frac{\theta_{i+1,j} - \theta_{i-1,j}}{2\Delta Y}$$

$$\frac{\partial^2 \theta}{\partial Y^2} = \frac{\theta_{i+1,j} - 2\theta_{i,j} + \theta_{i-1,j}}{\Delta Y^2}$$
(15)

and get the discretized form

$$A_{2}\theta_{i+1,j} - B_{2}\theta_{i,j} + C_{2}\theta_{i-1,j} = D_{2}$$
(16)
where

$$A_{2} = \frac{1}{P_{r}} + \frac{1}{2} \Delta Y \left(\frac{1}{2} Y_{j} U_{i,j} + V_{i,j} \xi_{i} \right)$$

$$B_{2} = - + - U_{i,j-i} + \Delta Y \ U_{i',j}$$

$$C_{2} = \frac{1}{P_{r}} - \frac{1}{2} \Delta Y \left(\frac{1}{2} Y_{j} U_{i,j} + V_{i,j} \xi_{i} \right)$$

$$D_{2} = - \frac{\Delta Y^{2}}{\Delta \xi} U_{i,j} \xi_{i} \theta_{i,j+1}$$
(17)

From this, we get a tri-diagonal system of algebraic equations, which is solved by using Gaussian elimination technique. The computational domain is of size 80×80 mesh points, and computational is started from $\xi = 0$ and march down implicitly, for this we have taken the step size $\Delta \xi$ =0.05 and ΔY =0.05. We calculate the effects of different parameters on coefficients of skin friction, rate of heat transfer, velocity and temperature field with the help of equations.

$$Re_{x}^{\frac{1}{2}}Cf_{x} = \left(\frac{\partial U}{\partial y}\right)_{y=0}, \quad Nu_{x}Re_{x}^{-\frac{1}{2}} = \left(\frac{\partial \theta}{\partial Y}\right)_{y=0}$$
(18)

and velocity can be calculated directly using equation of continuity (4) as shown below:

$$V_{i,j} = V_{i-1,j} - \frac{1}{2} \left(\xi \frac{\Delta y}{\Delta \xi} - Y_j \right) U_{i,j} + \frac{1}{2} \xi \frac{\Delta y}{\Delta \xi} U_{i,j-1} - \frac{1}{2} Y_j U_{i-1,j}$$
(19)

Stream function formulation

To get the set of equations in convenient form for integration, we define the following one parameter of transformations for the dependent and independent variables.

$$\psi = (2x)^{\frac{1}{2}} (1-x)^{\frac{1}{2}(1-\alpha)} G(x,\eta)$$

$$\eta = \frac{y}{(2x)^{\frac{1}{2}} (1-x)^{\frac{1}{2}(1-\alpha)}}$$

$$\theta = \frac{T - T_{\infty}}{T_{w} - T_{\infty}}$$
By using this group of transformations we have x and y components

of velocity as

$$u = (-x) G'$$

$$v = -\frac{(2x)^{\frac{1}{2}}(1-x)^{\frac{1}{2}(1-\alpha)}}{2x(1-x)} \left(2x(1-x)\frac{\partial G}{\partial x} + \eta(2x+\alpha x-1)G' - x(1-\alpha)G + (1-x)G\right)$$
(21)

Now the complete transformed form of the model of the problem attains the following form

$$G''' + 2\alpha x (1 - G'^{2}) + 2(1 - x)\lambda \theta - 2M(G' - 1) + (1 - 2x + \alpha x)GG''$$

$$= 2x(1-x)\left(G'\frac{\partial G'}{\partial x} - G''\frac{\partial G}{\partial x}\right)$$
(22)

$$\frac{1}{P_r}\theta'' - \theta'G(1 - 2x + \alpha x) = 2x(1 - x)\left(G'\frac{\partial\theta}{\partial x} - \theta'\frac{\partial G}{\partial x}\right)$$
(23)

with transformed boundary conditions

$$G(0) = 0, \quad G'(0) = 0, \quad \theta(0) = 1$$

 $G'(\infty) = 1, \quad \theta(\infty) = 0$ (24)

Local non-similarity method

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The solution of the set of locally non-similar equations can be obtained by using local Non- similarity method (LNS). The governing coupled Partial Differential equations are transformed into a sequence of coupled ordinary differential equations (ODE), which are then solved numerically. The local non-similarity method avoids this by deleting the stream-wise a derivative term, that is, the term with $\partial / \partial \xi$. This changes the partial differential equation (PDE) into non-linear ODE, that still has to be solved numerically. The local non-similarity method was first developed by Sparrow and Yu [6], Minkowycz and Sparrow [2] and later used by Chen [17] in his work.

To adopt this method, we first retain all terms in the transformed form with x derivative. Now the systems of equations that we have to

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solve by using LNS are equations (23) and (24).

Now by putting
$$F = \partial G / \partial x$$
 and $\varphi = \partial \theta / \partial x$ we have:

$$G'' + 2\alpha x \left(1 - G'^2\right) + (1 - 2x + \alpha x) GG'' + 2\lambda (1 - x) \theta + 2M (1 - G') = 2x (1 - x) (G'F' - G''F)$$
 (25) and

$$\frac{1}{P_r}\theta'' - (1 - 2x + \alpha x)G\theta' = 2x(1 - x)(G'\varphi - \theta'F)$$
(26)

With boundary conditions

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$$F(0) = 0, \quad F'(0) = 0, \quad \varphi(0) = 1$$

$$F'(\infty) = 1, \quad \varphi(\infty) = 0 \tag{27}$$

$$F'' - 4\alpha x GF' + 2\alpha (1 - G'') + (1 - 2x + \alpha x) (GF' - G'F) + (\alpha - 2) GG'' + 2\lambda (1 - x) \varphi - 2\lambda \theta = 2x (1 - x) (F'^2 - FF'') + 2(1 - 2x) (G'F' - G''F)$$
(28)

$$\frac{1}{P_r} \varphi'' - (1 - 2x + \alpha x) (G\varphi' + \theta') - (\alpha - 2) G\theta' = 2x(1 - x) (\varphi F' - F\varphi') + 2(1 - 2x) (G'\varphi - \theta'F)$$
(29)

With boundary conditions

$$F(0) = 0, \quad F'(0) = 0, \quad \varphi'(0) = 1$$

 $F'(\infty) = 1, \quad \varphi(\infty) = 0$ (30)

This is the second level of truncation of the Local Non-Similarity because this approximation is made by dropping terms in second level of equations. This system of coupled nonlinear ordinary differential equation now can be solved numerically by employing the Nachtsheim-Swigert [5] iteration technique in conjunction with the shooting procedure to determine the unknown boundary conditions f''(0) and $\theta'(0)$. Once we find the unknowns f''(0) and $\theta'(0)$, we are able to find the coefficients of skin friction and rate of heat transfer for different effects of parameters such as algebraic decay parameter α , Hartmann number M, Richardson parameter Ri and Prandtl number Pr with the help of following relations:

$$Re_{x}^{\frac{1}{2}}Cf_{x} = f''(\xi, 0), \qquad Nu_{x}Re_{x}^{-\frac{1}{2}} = \theta'(\xi, 0)$$
(31)

Results and Discussions

In this section we will discuss the results obtained by Finite Difference Method and Local Non- Similarity Method. In this study, we explore the effects of different parameters on coefficients of skin friction, rate of heat transfer, velocity field and magnetic field. With this understanding the Figures 2a and 2b presents the effects of different values of algebraic decay parameter α =0.01, 0.05, 0.1 by keeping other parameters constant on momentum and boundary layer thicknesses. From these figures it is possible to see how the algebraic decay parameter









 α =0.07 M=1.0, and for Prandtl number P_r=0.71. α influences the free stream velocity distribution at Y=16-18, and there

is no effects of algebraic decay parameter on temperature distribution. The reason is that if we see the equation (2) the algebraic decay is only the part of free stream velocity $U=(1-x) - \alpha$ outside the boundary so in both cases this parameter has its no effects within the boundary layer.

In Figures 3a and 3b, the influence of Prandtl number Pr (which is the ratio of kinematic viscosity to thermal diffusion) on momentum and thermal boundary layer thicknesses is shown. For increasing value of Prandtl number both the momentum and thermal boundary layer thicknesses are decreased with the reason that with the increase of Prandtl number Pr the fluid become more viscous which slow down the fluid motion, so distributions on both cases are decaying and this decay is asymptotic. Figures 4a and 4b show some results of variation of Richardson/mixed convection parameter R=1.0, 10.0, 20.0 on velocity and temperature profile. In this range of Richard parameter the momentum boundary layer thickness is decreased because the Richardson number acts like pressure gradient which take the responsibility of this physical phenomena but its effects in the case of thermal boundary layer is vice versa. Figures 5a and 5b shows the behavior of various values of Hartmann number M=1.0, 10.0, 20.0 on momentum and thermal boundary layer thicknesses. From this numerical exercise we can see the increase of applied magnetic field momentum boundary layer is decreased and thermal boundary layer is increased for maximum value of M=20.0.

Tables 1 and 2 shows some of the results obtained by Finite Difference Method and Local Non-Similarity method for different values of Hartmann number M on coefficient of skin friction and rate of heat transfer. From these tables, it is conclude that with the increase of Hartmann number M the coefficient skin friction and rate of heat transfer both are decreased. For increasing value of Hartmann number increase the magnetic energy and decrease the kinetic energy in the fluid flow domain due to this reason both quantities are decreased.



Figure 5: (a) velocity and (b) temperature field profile against boundary layer thickness Y for different values of Hartman number M=1.0, 10.0, 20.0 when α =0.07 R=1.0 and for Prandtl number P_r=0.71.

М	FDM	LNS
0.1	0.79478	0.79104
1.0	0.47204	0.47975
2.0	0.39717	0.37143
3.0	0.35781	0.34295
4.0	0.33172	0.33344
5.0	0.29738	0.29370
6.0	0.28504	0.27167
7.0	0.27465	0.25359
8.0	0.26571	0.22936

Table 1: Numerical values of coefficient of Skin friction $Re_x^{\frac{1}{2}}Cf_x$ obtained for different values of M when P_r=10.0, α =0.4, R_i=2.0.

М	FDM	LNS
0.1	0.58954	0.58320
1.0	0.36669	0.36761
2.0	0.31328	0.31274
3.0	0.28548	0.27415
4.0	0.26716	0.26240
5.0	0.25387	0.23197
6.0	0.24357	0.23177
7.0	0.223526	0.21319
8.0	0.22834	0.20981

Table 2: Numerical values of coefficient of rate of heat transfer $Nu_x Re_x^{-2}$ obtained for different values of M when P_r =10.0, α = 0.4, R_i = 2.0.

R	FDM	LNS
0.1	0.22415	0.22304
1.0	0.34958	0.34275
2.0	0.47204	0.46274
3.0	0.58357	0.57495
4.0	0.68803	0.68240
5.0	0.78664	0.78197
6.0	0.88073	0.86677
7.0	0.97108	0.91359
8.0	1.14268	1.0936

Table 3: Numerical values of coefficient of Skin friction $\frac{1}{Re_{\chi}^2 Cf_{\chi}}$ obtained for different values of R₁ when P_r =10.0, α =0.4, M=1.0.

The effects of different values of Richardson parameter on coefficients of skin friction and rate of heat transfer are shown in Tables 3 and 4. From these tables it can be seen that the skin friction and heat transfer are both increased because of the influence of the buoyancy force. The effects of various values of Prandtl number Pr on coefficients of skin friction and rate of heat transfer are shown in Tables 5 and 6.

R	FDM	LNS
0.1	0.28611	0.28014
1.0	0.33156	0.33975
2.0	0.36669	0.36743
3.0	0.39392	0.39214
4.0	0.41644	0.41238
5.0	0.43579	0.43184
6.0	0.45286	0.46671
7.0	0.46819	0.47347
8.0	0.49496	0.50304

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Table 4: Numerical values of coefficient of rate of heat transfer $Nu_x Re_x^{-\frac{1}{2}}$ obtained for different values of R₁ when P_r=10.0, α=0.4, M=1.0.

Ρ,	FDM	LNS		
0.1	0.48354	0.48201		
1.0	0.48197	0.48175		
2.0	0.48039	0.48143		
3.0	0.47898	0.47102		
4.0	0.47772	0.462240		
5.0	0.47658	0.46001		
6.0	0.47554	0.45177		
7.0	0.47458	0.45093		
8.0	0.47368	0.45016		

Table	5:	Numerical	values	of	coefficient	of	Skin	friction	$R_{a}^{\frac{1}{2}}Cf$	obtained	for
differe	nt v	alues of P,	when R _i	=2.	0, α=0.4, M	=1.	0.		$\operatorname{Re}_{\overline{X}} \mathcal{O}_X$		

Ρ,	FDM	LNS		
0.1	0.10516	0.10404		
1.0	0.14134	0.14963		
2.0	0.17772	0.17702 0.20495 0.23209		
3.0	0.20992			
4.0	0.23859			
5.0	0.26444	0.25970		
6.0	0.28801	0.27653		
7.0	0.30973	0.29359		
8.0	0.32993	0.31936		

Table 6: Numerical values of coefficient of rate of heat transfer $_{Nu_x Re_x^{-2}} \frac{1}{2}$ obtained for different values of P_r when R_i=2.0, α =0.4, M=1.0.

From these tables it is concluded that the component of skin friction is decreased while the component of rate of heat transfer is increased due to the reason that the product of density and thermal diffusion is decreased which enhance the rate of heat transfer in the fluid flow domain. At the end the numerical results obtained by both methods are found to be in good agreement.

Conclusion

In this article we have illustrated the effects of different parameters on some physical quantities such as skin friction, rate of heat transfer, momentum and thermal boundary layer thicknesses. The dimensionless local balance equations were solved numerically using a Finite Difference and Local Non-Similarity method by FORTRAN code. At the end, we summarize the following findings.

The algebraic decay parameter a influences the free stream velocity distribution at Y=16-18, and there is no effects of algebraic decay parameter on temperature distribution. For increasing value of Prandtl number Pr both the momentum and thermal boundary layer thicknesses are decreased with the reason that with the increase of Prandtl number Pr the fluid become more viscous which slow down the

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fluid motion, so distributions on both cases are decaying and this decay is asymptotic. With the increase of Richard parameter the momentum boundary layer thickness is decreased because the Richardson number acts like pressure gradient which take the responsibility of this physical phenomena but its effects in the case of thermal boundary layer is vice versa. With the increase of applied magnetic field momentum boundary layer is decreased and thermal boundary layer is increased for maximum value of M=20.0. For increasing value of Hartmann number increase the magnetic energy and decrease the kinetic energy in the fluid flow domain due to this reason both quantities are decreased. It is also noted that the skin friction and heat transfer are both increased because of the influence of the buoyancy force. It is also concluded that the component of skin friction is decreased while the component of the rate of heat transfer is increased due to the reason that the product of density and thermal diffusion is decreased which enhance the rate of heat transfer in the fluid flow domain.

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