

Effect of Constant Wall Permeability and Porous Media on the Creeping Flow through Round Vessel

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Abstract

The present study reports the influence of constant wall permeability and porous media on the creeping flow passing through round vessel. The inverse method is used to obtain the exact solution. To understand the behaviour of flow, the mathematical expression for stream function, velocity components, wall shear stress, pressure distribution, flow rate and leakage flux are provided. Our main purpose here is to demonstrate the constant permeability of the wall and of porous media on the existence of flow properties because of its applicability "flow through permeable renal disease tubule" in biological sciences. Flow properties at an entrance, mid place and at exit are discussed graphically for involved parameters and it is observed that low permeability of porous medium slow down the velocity of fluid along axial coordinate while minor change is observed along radial coordinate. While constant wall permeability shows the opposite behaviour on the same properties. Fractional permeation rate from the diseased vessel, wall permeation velocity, pressure drop and leakage flow rate are tabulated for physiological data of rat kidney. It is observed that for increasing wall permeability and high osmotic pressure drop provided maximum fractional permeation rate 84%. It is also noted that leakage flow and the amount of permeate fluid are independent of porosity of porous media, they only depend on the constant wall permeability. Comparison of the present study with the previous work in view of fractional permeation rate is also provided in the results section.

Keywords: Constant wall permeation; Porous media; Diseased renal tubule; Fractional permeation rate (FPR); Partial obstruction

Introduction

In past years, flow through porous media regime has been a subject of intensive study in a field of sciences with varying degree of success due to its important application in engineering, industry and medical fields. Production of petroleum and natural gasses, well drilling, lodging, fluid flow through obstructed renal tubules require many predictions based on results of fluid flow through a porous media. The motion of the fluid is affected by so many factors. The boundaries of the fluid affect the flow to have stationery boundaries, fluctuating boundaries, moving boundaries, oscillatory boundaries, porous boundaries and so on. The fluid motion in ducts, parallel plate channels, rectangular channels, parabolic boundaries, circular and cylindrical boundaries have been studied due to their natural existence.

There are many flows (gastric and circulatory) through which garbage or waste material may be deposited in the vessels (arteries, veins, renal tubules, capillaries, and intestine) and it leads to a diseased system [1,2]. Therefore, the normal vessel that contains porous media can be treated using the model which evaluates supplementary drag forces exerted on the flow due to the presence of solid matrix numbers emphasized by Khalid and Vafai [3]. These matrix numbers may be some kind of food item which cannot be digested, bacterial masses or fatty bunch. The viscosity of such materials will also be a cause of disturbance to the flow through the circular tube. Some numbers may causes of fully blockage and some partially. In partial blockage, some material allowed to pass through the blocked zone and this effectiveness can be a deal, modeled and analyzed as porous media regime. When the fatty and fibrous tissues are clotted in the wall lumen, its distribution acts like a porous medium. The general equation of motion for the flow of a viscous fluid through a porous media has been derived by Ahmadi and Manvi [4]. The porous material containing the fluid is, in fact, a non-homogenous media. For the sake of analysis, it is possible

to replace it with a homogenous fluid which has dynamic properties equivalent to the local averages of the original non-homogenous medium.

Homogenous fluid flow through the circular vessel with constant and variable permeable wall has its own status and proposed by many authors [5-20] in past and most recent years with a special application of flow through the kidney. Kidneys are most important re-absorption and filtration plant in the body. Each kidney contains millions of nephrons. Nephrons are functional unit of the kidney. They consist of the glomerulus and renal tubules which are originating from the tuft of the glomerulus. Renal tubules are involved in one of the most important and final stages of the nephron function: Clearing the end products of metabolism and maintaining the volume of the body fluids. The major portion of the tubular function is being carried out by the proximal renal tubule. The tubular epithelium is highly permeable to water and small solutes, to facilitate their re-absorption from glomerular filtrate. It is generally accepted that fluid is transported across the permeable wall by trans-boundary pressure drop (TPD) which includes osmotic pressure due to proteins and other solutes. Thus, it is expected that the hydrodynamic of renal flow play a significant role in understanding the nephron function. The proximal renal tubules are not uniform all along their length and the wall permeability may also vary in

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Received May 02, 2018; **Accepted** May 29, 2018; **Published** June 10, 2018

Citation: Siddiqui AM, Siddiqa S, Naqvi AS (2018) Effect of Constant Wall Permeability and Porous Media on the Creeping Flow through Round Vessel. J Appl Computat Math 7: 399. doi: [10.4172/2168-9679.1000399](https://doi.org/10.4172/2168-9679.1000399)

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different portions of the tube. It is, therefore, appropriate to consider a theoretical model for renal flow with non-uniform tube cross-section and variable wall permeability.

This work is the influence of past research on the flow through the healthy vessel, the affected (diseased) vessel is under consideration. The motive of this work is to extend the work [15] by taking round vessel with effects of porous media and constant wall permeability. Our model is similar to the renal tubule, therefore all results in the present work are related to this application along with physiological data of rat kidney. The axisymmetric coordinate is chosen according to the geometry of the problem. The hydrodynamics equations for creeping flow of viscous fluid passing through the porous media within the permeable vessel are transformed. Exact solutions are obtained with the help of inverse method [21-27]. Ana-lytic expressions are derived for axial and radial velocities, flow rate, pressure distribution, pressure drop, wall shear stress and leakage flux. Effects of porous media, wall permeability and entrance flow rate on the flow characteristics are visualized graphically. FPR %, wall permeability rate, pressure drop, leakage flux and comparison of the present study with the published work are tabulated in the result section. In the end, the detailed conclusion of this study is also provided.

Problem Formulation

Creeping flow of an incompressible viscous fluid passing through round vessel filled with porous media has been considered. Length and radius of the vessel are L and R. The flow dynamics are about axial and radial direction, therefore, the axisymmetric coordinates (r ; 0 ; z) are selected according to the geometry of the problem in which axial axis is along the axis of the vessel and radial axis is perpendicular to it. The wall re-absorption is assumed to be constant. The radial component of velocity given by $v_r(r; z)$ is due to the constant re-absorption at the wall and axial component $v_z(r; z)$ is an extension of the vessel along which the flow is symmetric. The governing equations for such flow are given by the following set of equations:

$$v = [v_r(\gamma; z); 0; v_z(\gamma; z)] \quad (1)$$

$$\frac{1}{\gamma} \frac{\partial}{\partial \gamma} (\gamma v_r) + \frac{\partial v_z}{\partial z} = 0 \quad (2)$$

$$\frac{\partial p}{\partial \gamma} = \mu \left(\frac{\partial^2 v_r}{\partial \gamma^2} + \frac{1}{\gamma} \frac{\partial v_r}{\partial \gamma} - \frac{v_r}{\gamma^2} + \frac{\partial^2 v_z}{\partial z^2} \right) - \frac{\mu}{k} v_r \quad (3)$$

$$\frac{\partial p}{\partial \gamma} = \mu \left(\frac{\partial^2 v_z}{\partial \gamma^2} + \frac{1}{\gamma} \frac{\partial v_z}{\partial \gamma} + \frac{\partial^2 v_z}{\partial z^2} \right) - \frac{\mu}{k} v_z \quad (4)$$

where $p(\gamma; z)$, μ , k , v_r , v_z , γ , z are the hydrostatic fluid pressure inside the vessel, the coefficient of viscosity, the permeability parameter, the velocity along radial direction, the velocity along axial direction, the radial coordinate, and the axial coordinate respectively. The appropriate boundary conditions of the problem are:

$$v_r = 0, \frac{\partial v_z}{\partial \gamma} = 0 \text{ at } \gamma = 0 \quad (5)$$

$$v_r = v_0, v_z = 0 \text{ at } \gamma = R$$

$$2\pi \int_0^R \lambda v_z(\gamma, z) d\gamma = Q_0 \text{ at } z = 0, \quad (6)$$

$$p = p_0 \text{ at } z = 0 \text{ and } p = p_L \text{ at } z = L$$

where v_0 wall permeability, Q_0 the entrance flow rate, p_0 the pressure at entrance and p_L the pressure at exit of vessel (Figure 1).

By elimination of pressure from eqn.(3) and eqn.(4); we arrived at:

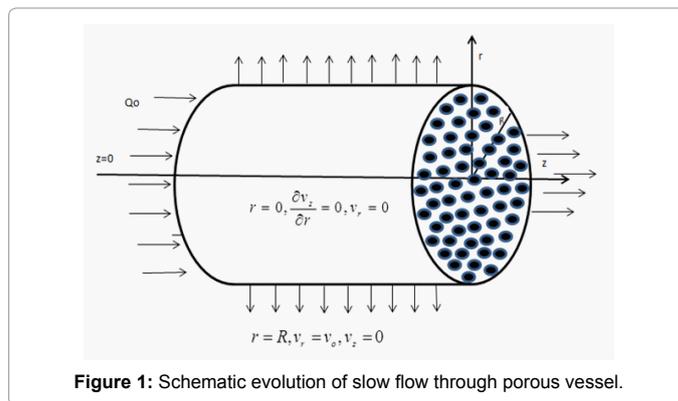


Figure 1: Schematic evolution of slow flow through porous vessel.

$$\frac{\partial}{\partial \gamma} \left\{ \frac{1}{\gamma} \frac{\partial}{\partial \gamma} \left(\gamma \frac{\partial v_z}{\partial \gamma} \right) \right\} + \frac{\partial^3 v_z}{\partial \gamma \partial z^2} - \frac{\partial}{\partial z} \left\{ \frac{\partial}{\partial \gamma} \left(\frac{1}{\gamma} \frac{\partial}{\partial \gamma} (\gamma v_r) \right) \right\} - \frac{\partial^3 v_r}{\partial z^3} + \frac{1}{k} \left(\frac{\partial v_r}{\partial z} - \frac{\partial v_z}{\partial \gamma} \right) = 0 \quad (7)$$

taking partial derivative of eqn.(7) with respect to z and using eqn.(2), we obtained:

$$\frac{\partial}{\partial z} \left[\frac{1}{\gamma} \frac{\partial}{\partial \gamma} \left\{ \gamma \frac{\partial}{\partial \gamma} \left(\frac{1}{\gamma} \frac{\partial}{\partial \gamma} \right) \right\} (\gamma v_z) + 2 \frac{\partial}{\partial \gamma} \left\{ \frac{1}{\gamma} \frac{\partial}{\partial \gamma} \left(\frac{\partial^2}{\partial z^2} \right) \right\} (\gamma v_r) + \frac{1}{\gamma} \frac{\partial^4}{\partial z^4} (\gamma v_r) + \frac{1}{k} \left\{ \frac{\partial}{\partial \gamma} \left(\frac{1}{\gamma} \frac{\partial}{\partial \gamma} \right) \right\} + \frac{1}{\gamma} \frac{\partial^2}{\partial z^2} \right] (\gamma v_r) = 0 \quad (8)$$

The velocity components in term of stream function $\psi(\gamma; z)$ are defined by:

$$v_r = \frac{1}{\gamma} \frac{\partial \psi}{\partial z}, v_z = -\frac{1}{\gamma} \frac{\partial \psi}{\partial \gamma} \quad (9)$$

Using eqn. (9), the eqn. (8) is finally reduces to the fourth order expression:

$$E^4 \psi - \frac{1}{k} E^2 \psi = 0 \quad (10)$$

or it can be re-written as:

$$E^2 (E^2 \psi) - \frac{1}{k} (E^2 \psi) = 0 \quad (11)$$

where the operator E^2 is defined as:

$$E^2 = \frac{\partial^2}{\partial \gamma^2} - \frac{1}{\gamma} \frac{\partial}{\partial \gamma} + \frac{\partial^2}{\partial z^2} \quad (12)$$

The transformed boundary conditions in term of stream function are:

$$\frac{\partial \psi}{\partial z} = 0, \frac{-1}{\gamma} \frac{\partial^2 \psi}{\partial \gamma^2} + \frac{1}{\gamma^2} \frac{\partial \psi}{\partial \gamma} = 0 \text{ at } \gamma = 0, \quad (13)$$

$$\frac{\partial \psi}{\partial z} = v_0 \gamma, \frac{\partial \psi}{\partial \gamma} = 0 \text{ at } \gamma = R \quad (14)$$

$$-\frac{Q_0}{2\pi} = \psi(R, z) - \psi(0, z) \text{ at } z = 0 \quad (14)$$

typically $\psi(0;0)=0$ so that eqn. (14) becomes:

$$-\frac{Q_0}{2\pi} = \psi(R, z) \text{ at } z = 0 \quad (15)$$

We finally obtain the bi-harmonic equation eqn. (11) along with non-homogenous boundary conditions eqns. (12-15), presenting creeping flow through the porous vessel with constant wall permeability.

Problem Solution

By proposing stream function of the form:

$$\psi(\gamma; z) = v_0 z f(\gamma) + g(\gamma) \quad (16)$$

where $f(\gamma)$ and $g(\gamma)$ are arbitrary functions. Using above assumption in eqns. (11-15); the following two differential equations in term of arbitrary functions are retrieved:

$$\left(\frac{\partial^2}{\partial \gamma^2} - \frac{1}{\gamma} \frac{d}{d\gamma}\right) \left\{ \left(\frac{d^2}{d\gamma^2} - \frac{1}{\gamma} \frac{d}{d\gamma}\right) - \frac{1}{k} \right\} f(\gamma) = 0 \quad \left(\frac{d^2}{d\gamma^2} - \frac{1}{\gamma} \frac{d}{d\gamma}\right) \left\{ \left(\frac{d^2}{d\gamma^2} - \frac{1}{\gamma} \frac{d}{d\gamma}\right) - \frac{1}{k} \right\} g(\gamma) = 0 \quad (17)$$

Associated boundary conditions are:

$$\frac{f(\gamma)}{\gamma} = 0, \frac{d}{d\gamma} \left(\frac{1}{\gamma} \frac{d}{d\gamma} \right) f(\gamma) = 0, \frac{d}{d\gamma} \left(\frac{1}{\gamma} \frac{d}{d\gamma} \right) g(\gamma) = 0 \text{ at } \gamma = 0 \quad (18)$$

$$\frac{f(\gamma)}{\gamma} = 1, \frac{df(\gamma)}{d\gamma} = 0, \frac{dg(\gamma)}{d\gamma} = 0 \text{ at } \gamma = R \quad (19)$$

$$g(R) - g(0) = \frac{-Q_0}{2\pi} \text{ at } z = 0 \quad (20)$$

The solution of Eq. (17) is:

$$f(\gamma) = \frac{2\gamma I_1\left(\frac{\gamma}{\sqrt{k}}\right) - \frac{\gamma^2}{\sqrt{k}} I_0\left(\frac{\gamma}{\sqrt{k}}\right)}{2I_1\left(\frac{R}{\sqrt{k}}\right) - \frac{R}{\sqrt{k}} I_0\left(\frac{R}{\sqrt{k}}\right)} \text{ and } g(\gamma) = -\frac{Q_0}{2\pi R} \frac{2\gamma I_1\left(\frac{\gamma}{\sqrt{k}}\right) - \frac{\gamma^2}{\sqrt{k}} I_0\left(\frac{\gamma}{\sqrt{k}}\right)}{2I_1\left(\frac{R}{\sqrt{k}}\right) - \frac{R}{\sqrt{k}} I_0\left(\frac{R}{\sqrt{k}}\right)} \quad (21)$$

where I_1, I_2 are modified bessel functions [21] of order 1 and 2: The expression for stream function is obtained as:

$$\psi(\gamma, z) = v_0 \frac{2\gamma I_1\left(\frac{\gamma}{\sqrt{k}}\right) - \frac{\gamma^2}{\sqrt{k}} I_0\left(\frac{\gamma}{\sqrt{k}}\right)}{2I_1\left(\frac{R}{\sqrt{k}}\right) - \frac{R}{\sqrt{k}} I_0\left(\frac{R}{\sqrt{k}}\right)} - \frac{Q_0}{2\pi R} \frac{2\gamma I_1\left(\frac{\gamma}{\sqrt{k}}\right) - \frac{\gamma^2}{\sqrt{k}} I_0\left(\frac{\gamma}{\sqrt{k}}\right)}{2I_1\left(\frac{R}{\sqrt{k}}\right) - \frac{R}{\sqrt{k}} I_0\left(\frac{R}{\sqrt{k}}\right)} \quad (22)$$

both radial and axial velocity components are respectively obtained as:

$$v_r(\gamma, z) = v_0 \frac{2I_1\left(\frac{\gamma}{\sqrt{k}}\right) - \left(\frac{\gamma}{\sqrt{k}}\right) I_0\left(\frac{\gamma}{\sqrt{k}}\right)}{2I_1\left(\frac{R}{\sqrt{k}}\right) - \frac{R}{\sqrt{k}} I_0\left(\frac{R}{\sqrt{k}}\right)} \text{ and } v_z(\gamma, z) = -\frac{1}{\sqrt{k}} I_0\left(\frac{\gamma}{\sqrt{k}}\right) - \frac{1}{\sqrt{k}} I_0\left(\frac{R}{\sqrt{k}}\right) \left\{ 2v_0 z - \frac{Q_0}{\pi R} \right\} \quad (23)$$

The longitudinal (axial) flow rate denoted by $Q(z)$ and leakage or rate after straight forward computation are given as respectively:

$$Q(z) = \int_0^R 2\pi r v_z(\gamma, 0) dr = Q_0 - 2\pi R v_0 z \quad (24)$$

$$q(z) = \frac{dQ(z)}{dz} = 2\pi R v_0 \quad (25)$$

The expression for pressure distribution in the vessel by the cross integration of eqn.(3) and eqn. (4) yields the solution for $p(\gamma; z)$ in term of r and z ; the average pressure of fluid at end point, pressure drop over the length L of the leaky vessel and wall shear stress at wall are respectively given below:

$$\frac{1}{\mu} p(\gamma, z) = 2v_0 \frac{1}{\sqrt{k}} I_0\left(\frac{\gamma}{\sqrt{k}}\right) - \frac{1}{\sqrt{k}} I_0\left(\frac{R}{\sqrt{k}}\right) + \left(v_0 z - \frac{Q_0}{\pi R}\right) \frac{z}{(k)^{3/2}} I_0\left(\frac{\gamma}{\sqrt{k}}\right) + \frac{p_0}{\mu} \quad (26)$$

$$\bar{p}(z) = \frac{\int_0^R p(\gamma, z) 2\pi r d\gamma}{\int_0^R 2\pi r d\gamma} = \frac{2v_0 \mu}{R} + \frac{2\mu z}{kR^2} \left(v_0 z - \frac{Q_0}{\pi R}\right) \frac{I_1\left(\frac{R}{\sqrt{k}}\right)}{2I_1\left(\frac{R}{\sqrt{k}}\right) - \frac{R}{\sqrt{k}} I_0\left(\frac{R}{\sqrt{k}}\right)} \quad (27)$$

$$\Delta \bar{p} = \bar{p}(0) - \bar{p}(L) = -\frac{2\mu L}{kR^2} \left(v_0 L - \frac{Q_0}{\pi R}\right) \frac{I_1\left(\frac{R}{\sqrt{k}}\right)}{2I_1\left(\frac{R}{\sqrt{k}}\right) - \frac{R}{\sqrt{k}} I_0\left(\frac{R}{\sqrt{k}}\right)} \quad (28)$$

$$\tau_\gamma = R = -\mu \left(\frac{\partial v_z}{\partial \gamma} + \frac{\partial v_\gamma}{\partial z} \right) = -\frac{\frac{\mu}{k} I_1\left(\frac{R}{\sqrt{k}}\right)}{2I_1\left(\frac{R}{\sqrt{k}}\right) - \frac{R}{\sqrt{k}} I_0\left(\frac{R}{\sqrt{k}}\right)} \left(2v_0 z - \frac{Q_0}{\pi R} \right) \quad (29)$$

The amount of permeate fluid from the wall of circular vessel can be defined as fractional permeation rate [15]. It can be computed as:

$$FPR = \frac{Q(0) - Q(L)}{Q(0)} = \frac{2\pi R v_0 L}{Q_0} \quad (30)$$

which shows the dependence of FPR on constant wall permeability v_0 (re-absorption velocity) and axial flow rate Q_0 .

Results and Discussion

In this section, results are analysed in two ways; one is the theoretical results which are generated by Mathematica for varying one flow parameter and fixing others, and other is physiological results i.e., done for all relevant values of physiological situation. Introducing non-dimensionalization for the convenience of the graphical representation:

$$\gamma^* = \frac{\gamma}{R}, z^* = \frac{z}{R}, v^* = \frac{v}{U}, p^* = \frac{p}{\mu U / R}, k^* = \frac{k}{R^2} \quad (31)$$

where U is the fluid entrance velocity. All the results are predicted along different axial positions namely; Entrance ($z=0:1$), middle ($z=0:3$) and exit of the vessel ($z=0:6$) for the length of vessel equals to 0:67. In Figure 2, radial velocity increases for increasing permeability parameter of porous media but remains symmetric at all position downstream due to constant permeation. Figure 3 depicted the increasing behavior of

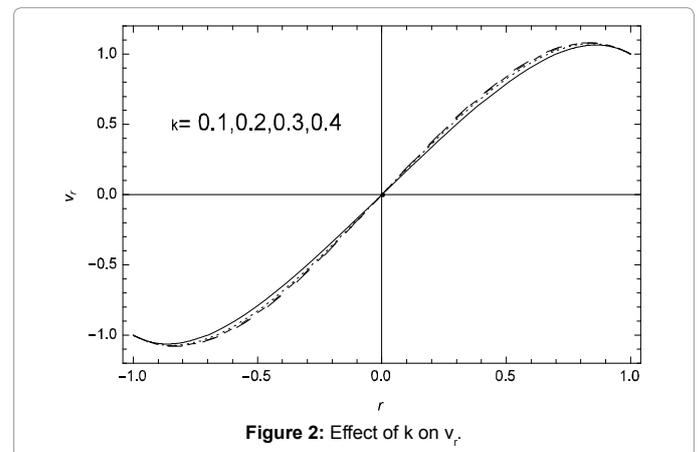


Figure 2: Effect of k on v_r .

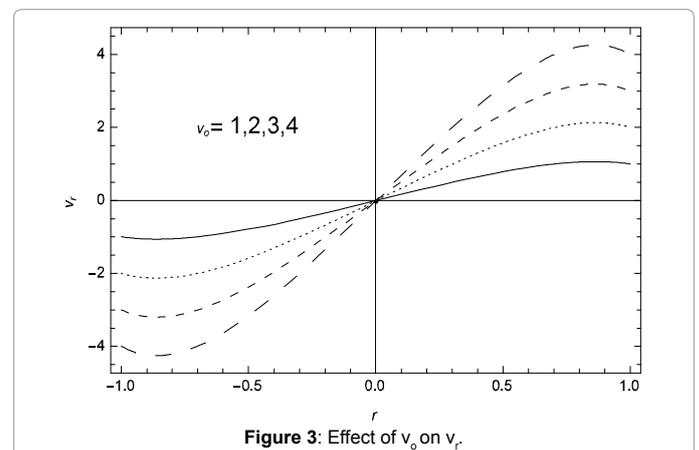
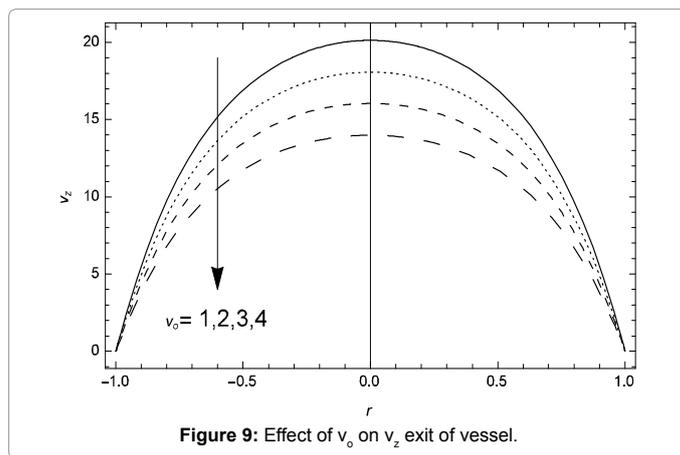
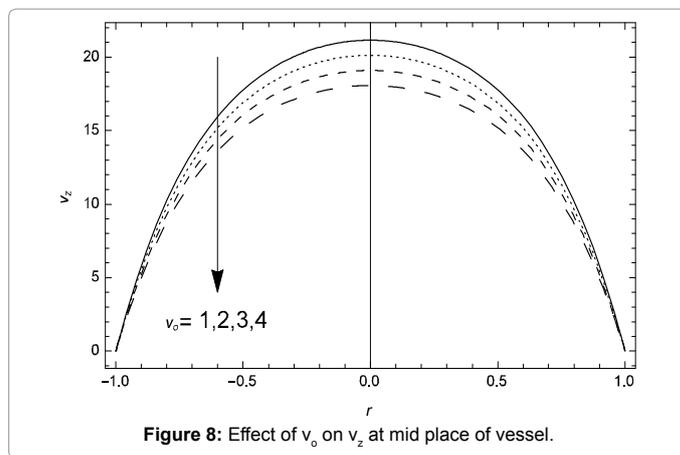
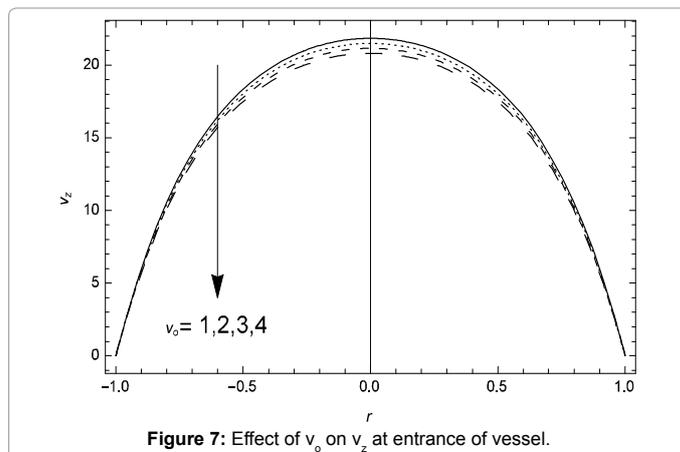
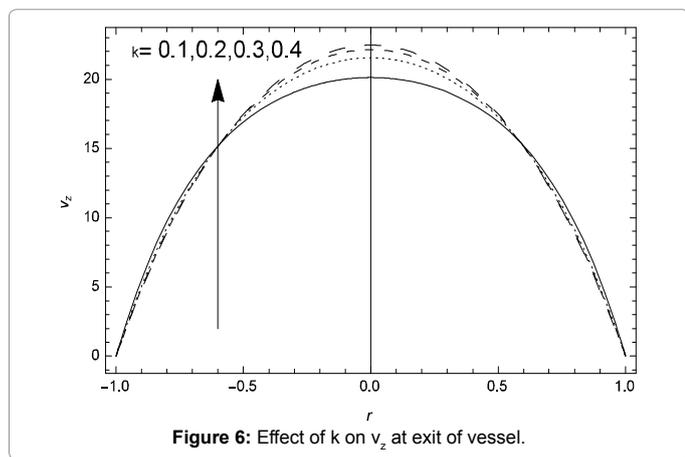
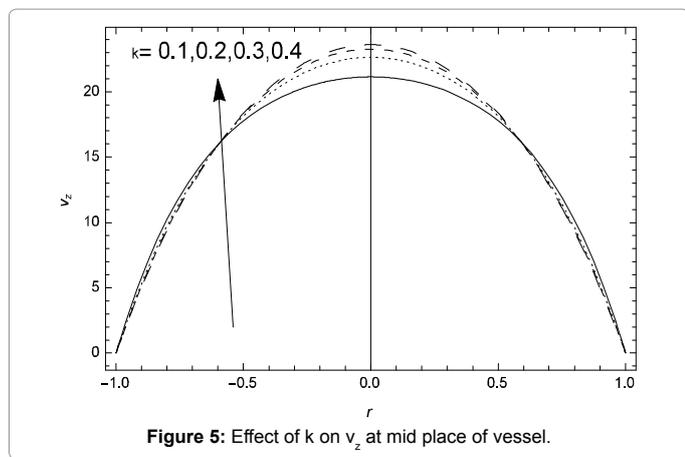
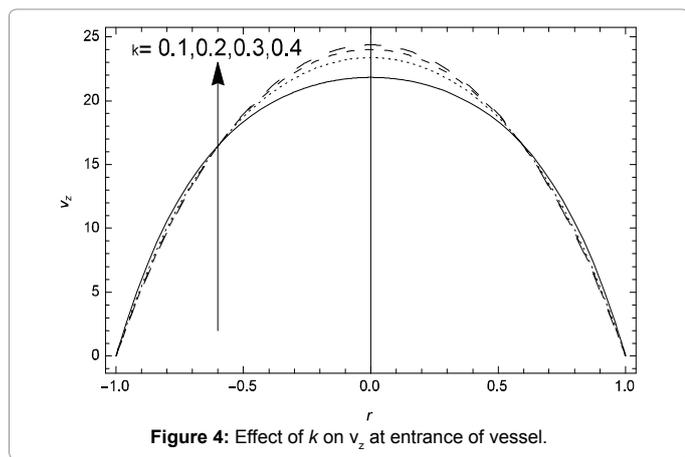


Figure 3: Effect of v_0 on v_r .

radial velocity for increasing rate of wall permeation velocity v_o . Figures 4-6 is plotted against the increasing values of permeability k of porous media on the axial velocity at the entrance, mid place and exit of the vessel. It is observed that axial velocity gradually increases when the permeability k increases. Axial velocity decreases for increasing wall permeation velocity v_o , (Figures 7-9). From Figures 10 and 11 showed that vessel hydrostatic pressure distribution increases linearly for increasing k and v_o .

For theoretical and experimental point of view, physiological data of rat kidney is given in Table 1. Variation in F P R for different



values of wall permeability, pressure drop, and leakage flux has been given in Table 2 with the help of physiological data provided in Table 1. It is observed that for increasing wall permeability, pressure drop and leakage flow rate the F P R through walls attained its maximum value for the case of the constant rate of permeation at the wall. Table 3 shows the comparison of F P R% with previous work [15]. It is observed that the percentage of fractional permeation rate difference with experimental data of rat kidney is higher in diseased vessel than the healthy vessel.

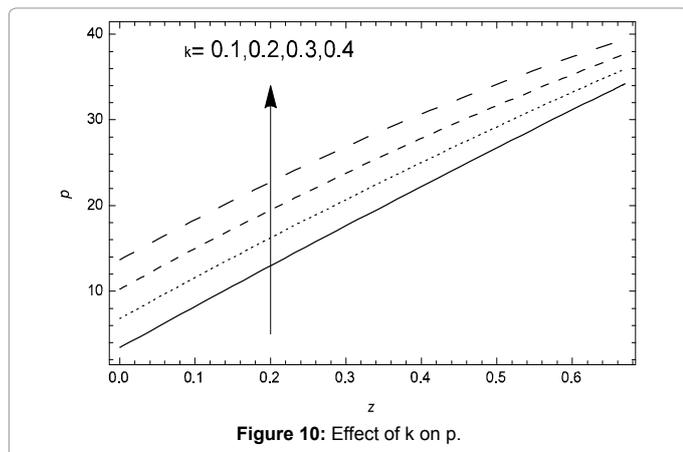


Figure 10: Effect of k on p.

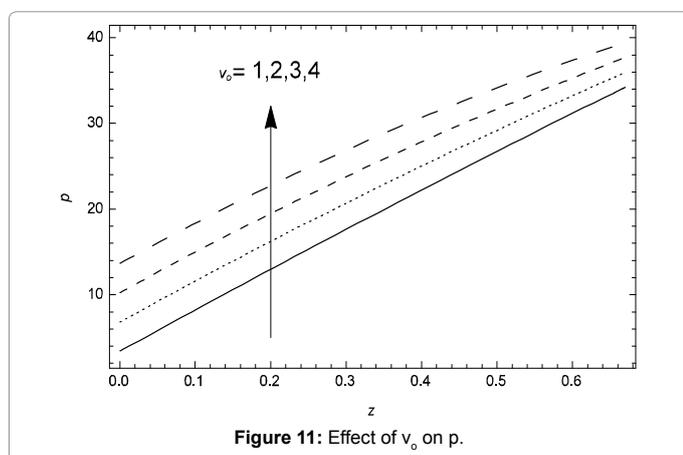


Figure 11: Effect of v₀ on p.

Quantity	Symbols	Values	Units
Radius tube	R	0.00108	Cm
Length Tube	L	0.67	Cm
Entrance Pressure	P _c	14400.	$\frac{dYn}{cm^2}$
Entrance Flow Rate	Q ₀	4.08×10 ⁻⁸	$\frac{cm^2}{sec}$
Viscosity	μ	0.00737	$\frac{dYn.sec}{cm}$

Table 1: Physiological data for the rate kidney.

FAR%	Wall permeability*10 ⁻⁴	Pressure drop*10 ⁶	Leakage flow rate *10 ⁻⁶
84	1.6	-4.29842	1.08573
78	1.5	-4.49296	1.01788
73	1.4	-4.6875	0.95002
68	1.3	-4.88204	0.88216

Table 2: Variation of fractional permeation rate FPR, for different values of wall permeation velocity, pressure drop and leakage flow rate.

FPR%	FPR difference with experimental data%	Flow	Assumed Geometry	Status of renal tubule
80	7	Homogenous regime	Parallel plates	healthy
84	11	Medium porous regime	Round vessel	Diseased

Table 3: FPR% difference with experimental value that is 73% for the constant wall permeation v₀=1:6.

Conclusion

Here we have supposed wall permeability of round vessel as a constant function of axial distance. The vessel is filled with some waste material which is playing a role of porous media. Results are interpreted against the effect of porous media and constant wall permeation. Physiological data of rat kidney is used to interpret the results. Important conclusions are as followed: When the porosity of media is higher, then fluid will stay longer in the vessel and hence the percentage of FPR will increases (that is 84%) and its difference with actual experimental results is 11%. This study stated the swear condition of the diseased permeable vessel (leaky diseased renal tubule). The previous findings can be obtained by setting: permeability parameter (k) of porous media approaches to infinity, we can obtain the solution of the homogenous fluid regime with constant wall permeability [9]. It is also observed that if wall permeability (v₀) approaches to zero and parameter (k) approaches to infinity then classical results of Poiseuille flow (homogenous fluid regime with impermeable boundary) can be achieved. If v₀ approaches to zero but k is set to be free then flow through porousmediaregime with a homogenous wallisretrieved where nopermeation has been taken from the walls of the vessel. Since constant wall permeability of vessel is not the ideal case, thus the present model may be improved by taking appropriate variable wall permeability of round vessel filled with some partial obstruction.

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