

SO₂ Emission Control and Finding a Way Out to Produce Sulphuric Acid from Industrial SO₂ Emission

Papiya Roy^{1*} and Arghya Sardar²

¹University of Guelph, Guelph, Canada

²Technology Information, Forecasting and Assessment Council (TIFAC), India

Abstract

Sulphur dioxide (SO₂) is one of a group of highly reactive gases known as “oxides of sulphur”. SO₂ is linked with a number of adverse effects on the respiratory system and other environmental issues. It is an important industrial emission gas which causes several difficulties in the environment like acid rain. Sulphur dioxide is a ubiquitous component of fuel combustion exhausts and one of the first air pollutants to be regulated all over world. Several approaches have been adopted to reduce SO₂ content in the environment. One of the most difficult environmental problems facing industry is how to economically control SO₂ emissions. Conversion of H₂SO₄ from SO₂, which could be a great impact on reducing pollution. Production of sulphuric acid is one of the best choice considering its economical values and utilities. This paper addresses the different processes to control SO₂ and to use SO₂ in most economic and productive way to reduce SO₂ effect in environment. A review of various treatment methods has been provided and a brief description of each process has been included and their technical applicability is also compared.

Keywords: Sulphuric acid; Sulphur dioxide; Scrubber; Reduction; Oxidation

Introduction

Six common air pollutants were identified as criteria pollutants in the Clean Air Act of 1970. Sulphur dioxide (SO₂) is one of them, the other five being carbon monoxide, lead, nitrogen dioxide, ozone and particulate matter. High level of sulphur dioxide emission is associated with various ecological damages and health problems. Sulphur dioxide is harmful to health and it also contributes to acidification of soil and water. The major health issues are respiratory illness, breathing difficulties etc. [1]. Short-term exposure to SO₂ may cause wheezing, chest tightness and shortness of breath. Longer-term exposure to sulphur dioxide in conjunction with high levels of particulate soot may result in respiratory illness, alterations in the lungs' defenses and aggravation of existing cardiovascular disease. The environmental effects of SO₂ are detrimental. It reacts on the surface of a variety of airborne solid particles. It is soluble in water and can be oxidized within airborne water droplets to form sulphuric acid (H₂SO₄), which falls as acid precipitation, or “acid rain”. Acid rain pollutes and acidifies the soil.

Combustion of conventional fuels i.e. hard coal and brown coal, oil and natural gas cause pollution of the atmosphere with sulphur oxides (SO₂ and SO₃), nitrogen oxides (NO_x) and dust. Discontinuing use of these energy sources in the nearest future seems unlikely. Hence, the only acceptable solution is application of appropriate technologies and equipment eliminating substances hazardous for the environment formed from fuels or after combustion of waste gases. The emission of SO₂ from coal-fired boilers is regulated strictly in many countries. The increase in coal uses will also result in an increase in sulphur dioxide emission. There are many methods available for controlling the emission of SO₂ of coal-fired boilers. Methods of removing SO₂ from boiler and furnace exhaust gases have been studied for over 150 years. Tall flue gas stacks disperse emissions by diluting the pollutants in ambient air. Once SO₂ is released into the atmosphere, it may be converted to other compounds and/or removed from the atmosphere by various mechanisms. Processes such as oxidation, wet deposition, dry deposition, absorption by vegetation and by soil, dissolution into water and other processes contribute to the removal of SO₂ from the atmosphere. As recent environmental concern enforces more strict

regulations of the emission of SO₂, the treatment of SO₂ in flue gas has attracted increasing attention. So the approaches to address this issue have been to reduce emission of SO₂ as well as conversion of SO₂ to sulphuric acid. Historically, there has been a multitude of processes for SO₂ emission control.

In flue gas cleaning processes, SO₂ is usually removed by absorption with lime (CaOH₂·2H₂O) or other compounds having high alkalinity. State-of-the-art desulphurization can remove more than 98% of the SO₂ from the flue gas. SO₂ is therefore removed from the atmosphere either unchanged or in the form of sulphuric acid and sulphates. The conversion of SO₂ to sulphuric acid and sulphates represents approximately 10% of the rate of removal of SO₂ from the atmosphere. The different process of sulphur dioxide removal from various sulphur operations and production of sulphuric acid from this SO₂ is studied in this paper. It presents a detailed overview of the trends in control of SO₂ emissions from industrial sources and also discusses technologies for production of sulphuric acid from SO₂ emission. Broadly, the following discussions are presented in five sections. (1) Various sources of SO₂ emissions are discussed. (2) Detailed overview of various approaches for SO₂ emission control. (3) Selection of appropriate flue-gas desulphurisation technique. (4) Trends in the technologies for recovery of sulphuric acid from SO₂ emission (5) Conclusion.

Sources of Sulphur Dioxide

Sulphur dioxide and nitrogen oxides are regulated air pollutants. They are usually emitted from industrial, transportation and domestic activities and in many occasions simultaneously. Sulphur dioxide is introduced in environment as a result of both natural phenomena and

*Corresponding author: Papiya Roy, University of Guelph, Guelph, Canada. Tel: 913324742323, E-mail: papiya.roy@gmail.com

Received April 20, 2015; Accepted May 30, 2015; Published June 10, 2015

Citation: Roy P, Sardar A (2015) SO₂ Emission Control and Finding a Way Out to Produce Sulphuric Acid from Industrial SO₂ Emission. J Chem Eng Process Technol 6: 230. doi:10.4172/2157-7048.1000230

Copyright: © 2015 Roy P, et al. This is an open-access article distributed under the terms of the Creative Commons Attribution License, which permits unrestricted use, distribution, and reproduction in any medium, provided the original author and source are credited.

anthropogenic activities such as combustion of fossil fuels, oxidation of organic material in soil, volcanic eruptions, biomass combustion etc. [2]. Fossil fuels, including coal, oil and to a lesser extent gas, contain sulphur both in organic and inorganic form. Urbanization and industrialization contribute to the addition of SO₂ in environment. Also meteorological condition affects significantly the amount of SO₂ in environment.

The largest sources of SO₂ emissions are from fossil fuel combustion at power plants (73%) and other industrial facilities (20%). In a thermal power plant SO₂ is generally produced when sulphur containing fuel is combusted. Smaller sources of SO₂ emissions include industrial processes such as extracting metal from ore, and the burning of high sulphur containing fuels by locomotives, large ships, and non-road equipment.

All conventional fossil fuels contain various sulphur bound organic and inorganic compounds and their sulphur content present as follows:

- Wood and cellulose rich biomass (<0.1 %)
- Natural gas (0-15 percent)
- Crude oil (0.3 to several percent)
- Coal (0.5 to >3.0 percent)

Fossil fuels like coal and crude oil deposits typically contain 1-2% sulphur by weight [3]. Combustion of fossil fuel thus is the major cause of anthropogenic emission of SO₂ in the environment. SO₂ is derived from various plants with other gases, like coal power plant, furnace off gases, sulphuric acid plants, cement industry, ship emission etc. [1,4-7]. The cargo and passenger ships sailing on sea routes were the largest sources of SO₂ along with other pollutants like NO_x and PM emissions of waterborne traffic in Finnish and nearby sea and lake areas in 2000.

Sulphur dioxide is found in many industrial gases emanating from plants involved in roasting, smelting and sintering sulphide ores, or gases from power plants burning high sulphur coal or fuel oils or other sulphurous ores or other industrial operations involved in the combustion of sulphur-bearing fuels, such as fuel oil. One of the more difficult environmental problems facing industry is how to economically control SO₂ emissions from these sources.

Approaches and Strategies for SO₂ Emission Control

Various methods for SO₂ control are based on either prevention of SO₂ pollution or end-of-pipe treatment of flue gases. But small-scale flue gas cleaning is often impractical and not feasible; substitution of sulphur-containing fuels by clean fuel is desirable. Various approaches for controlling SO₂ emissions include [8]:

- Use of clean fuel: This includes either switching to a fuel with reduced amount of sulphur or else a reduction of fuel-sulphur before its firing. Since SO₂ emissions are directly proportional to the sulphur content of fuel, and also to the amount of fired, a reduction in emissions can be achieved by switching to low-sulphur fuels and to higher quality ones.
- Removal of sulphur from the fuel: This includes coal washing. Hence various cleaning methods have been developed for desulphurizing sulphur-bearing fuels prior to their firing. Sometimes this is associated with changes in the physical characteristic of the fuel, resulting in operational problems.
- Preventing production and release of SO₂ during combustion: Several technologies have been developed to control SO₂

emission during combustion, however only few of them have been commercialized. The most developed are the fluidized bed combustion and integrated gasification combined cycle (IGCC).

- Flue gas desulphurization: The end-of-pipe treatment is based on flue gas desulphurization (FGD). The flue gas is treated before it is emitted into the atmosphere via the stack.

All of these methods can be used separately, or in conjunction with each other, depending on the quality of the fuel and the emissions requirements. The immediate focus of this paper is on flue gas desulphurisation (FGD) process. FGD technology is used to remove SO₂ from exhaust flue gases. FGD systems have been installed and operated on many industrial and utility boilers and on some industrial processes for a number of years [9]. These systems are capable of removing approximately 70 to 90% of the SO₂ in the flue gas, depending on the operating conditions of the system. Some systems have achieved an SO₂-removal efficiency of greater than 95%.

FGD technique offers several advantages such as:

- Effect of concentration: Fuel contains sulphur in a more concentrated solid or liquid form; in flue gas it is considerably diluted by nitrogen and excess combustion air.
- Effect of scale: Using clean fuel, desulphurized at refineries is simpler than installing pollution control at each small or medium-sized plant.
- Resource conservation: Desulphurization separates sulphur from fuel, yielding elemental sulphur that is marketable, easily recovered, shipped and handled.

Classification of FGD systems

In order to minimise the adverse effects of sulphur dioxide and sulphur trioxide on the environment, many power plants and industrial facilities use flue gas desulphurisation (FGD) scrubbers to remove SO₂ and SO₃ from combustion gases. Flue gas desulphurization systems can be broadly categorized as (1) Throw away or once through and (2) Recovery systems or regenerative system. In the throwaway systems, the sulphur removed from the flue gas is rejected from the process in a waste sludge [10]. In recovery systems, the sulphur-absorbing reagent is regenerated for recirculation to the flue gas contacting device and the sulphur removed from the flue gas is converted into its elemental form or into sulphuric acid.

Both once-through and regenerative technologies can be classified into wet and dry types. The wet processes involve production of wet slurry wastes as by products. The flue gas leaving the absorbent is saturated with moisture. Regenerative systems use expensive sorbents that are recovered by stripping sulphur oxides from the scrubbing medium. These produce useful by products including sulphur, sulphuric acid and gypsum. Recovery systems have generally higher capital costs than throwaway systems but lower waste disposal requirements and costs. The dry processes produce dry waste material and the flue gas leaving the absorbent is not saturated with moisture. SO₂ recovery efficiency of the dry processes (50-60%) is considerably less than the wet ones (93-98%) [9,11]. However, in recent times dry processes with more than 90% SO₂ removal efficiency are available.

Wet scrubber: In the wet scrubbing technique, slurry of an alkaline chemical reagent is used to absorb SO₂, and the gaseous SO₂ is converted into either a liquid or solid by product. The dominant choices for commercial installations have been the wet, throwaway (lime/limestone) systems.

Lime/limestone scrubbing: There are several types of wet non-regenerative processes. Among these lime/limestone scrubbing is the most popular. Frequently, limestone is used as the sorbent, generating gypsum as a by-product. Usually counter current vertical oriented spray tower is used as absorbent application. When the fraction of the CaSO₄ is more than 15%, gypsum scale is formed. The lime stone forced oxidation (LSFO) process prevents this scale formation by forcing oxidation of CaSO₃ to CaSO₄ by blowing air into the reaction tank or into an additional hold tank.

In the United States, over 90% of U.S. flue gas desulphurization system capacity uses lime or limestone. This trend will likely continue into the next phase of federally mandated SO₂ reduction from coal burning power plants. These are about 80% of the market share and are used in large utility boilers. This is due to the high SO₂ removal efficiency achieved and low costs involved.

Limestone/gypsum system: Globally the most commonly used flue gas desulphurization system is based on limestone/gypsum system. It involves mixing of crushed limestone/lime with water to form a slurry and spraying it into the sulphur containing flue gases. The sorbent reacts with SO₂ and forms an aqueous slurry of calcium sulphite. About 90% SO₂ removal can be achieved. Limestone-gypsum wet flue gas desulphurization method is most widely accepted due to its efficiency and reliability [12].

Sodium (hydroxide) scrubbing: The throw away sodium FGD systems have been used mostly on industrial boilers. These systems use a sodium scrubbing liquor that is very efficient in absorbing SO₂ emissions. They produce liquid wastes that can cause waste disposal problems. FGD systems used on utility boilers generate large quantities of liquid wastes. Therefore, throwaway-sodium systems have mainly been used on industrial boilers.

Ammonia scrubbing: Ammonia is used as a reagent and by product is ammonium sulphite, which can be used as a fertilizer. Based on extensive operation of this process, several advantages have been reported by Evans et al. [2009] [13]. Unlike the calcium based wet FGD, no CO₂ is produced in this process, and waste water discharge is also minimized. Scaling or blockage problems are unlikely. However, high capital cost and a large footprint are the disadvantages [13].

Seawater scrubbing process: Due to its natural alkalinity, seawater can absorb acidic gases. In this process, flue gases flow counter current to seawater in an absorption tower. The sea water gets heated and the flue gas is cooled. SO₂ in the flue gases is absorbed by the sea water and then passes to a water treatment plant where further seawater is added to increase the pH. Air is supplied to oxidize the SO₂ to sulphite and to saturate the seawater with oxygen. This system can remove up to 99% SO₂. There is no disposal of waste to the land, but heavy metals and chlorides are present in the water released to the sea. Sea water scrubbing has found application in coal and oil-fired power plants, metal smelters, oil refineries, petrochemical industries and chemical processing plants. However, this process is suitable only for plants in the coastal area.

Magnesium oxide: Magnesium oxide (MgO) slurry is sometimes used as an alternative. SO₂ absorbed in the scrubber slurry forms insoluble magnesium sulphite (MgSO₃), which is oxidized by injected oxygen to form MgSO₄. MgSO₃ and MgSO₄ are used in acid plants to produce SO₂ for sulphuric acid production.

Magnesium hydroxide: This process can achieve higher than 98% SO₂ removal efficiency, and is compact, simple and involve

less equipment [14]. Hence it has a low capital cost. Its use is much widespread in Japan.

Spray dry system: Slurry of alkali sorbent is injected into the flue gases in a fine spray. Usually slaked lime is used as alkali sorbent. The water evaporates due to heat from the flue gases, and the flue gases get cooled. SO₂ in the flue gases reacts with the drying sorbent to form a solid reaction product. No waste water is produced in this process.

Circulating dry scrubber (or fluidized bed FGD): It has high SO₂ removal efficiency with extremely low water consumption. It has the ability to bridge the size gap between spray dryer absorber and wet FGD technology.

Wet regenerative processes

Wet regenerative processes include Wellman-Lord Process and DESONOX processes. The basic principles of the Wellman Lord process consist of removing highly diluted SO₂ from the flue gas in the absorption section and then turning it into rich SO₂ gas in the regeneration section. In the absorption stage, ash, hydrogen chloride, hydrogen fluoride and SO₃ are removed as the hot flue gases are passed through a pre-scrubber. The gases are then cooled and fed into the absorption tower where a saturated solution of sodium sulphite is sprayed from the top onto the flue gases, which reacts with the SO₂ to form sodium bisulphite. The concentrated bisulphite is then collected and passed to an evaporation system for regeneration. In the regeneration stage, steam is used to break down sodium bisulphite. The sodium sulphite produced is recycled back to the flue gases.

Wellman-Lord FGD systems have been used to reduce SO₂ emissions from utility and industrial boilers and from a number of industrial processes. These systems have the advantage of regenerating the scrubbing liquor and producing a saleable product instead of a sludge that can be a disposal problem. However, these systems are more expensive to install and operate than lime, limestone, or dual-alkali systems. The DESONOX process is a combined catalytic process by which nitrogen oxides and sulphur dioxide are separated from the flue gas. Sulphuric acid is obtained as the final product which can be used in the chemical industry. Residual dust and aerosols are also collected from the flue gas.

Dual alkali: A sodium hydroxide and sodium sulphite solution is used in the scrubbing system. Reaction of this solution with SO₂ produces a solution of sodium bisulphite and sodium sulphite. This reacts with lime or limestone outside the scrubber to produce a precipitate of calcium salts containing calcium sulphite. After dewatering the solids are disposed of in a landfill. The liquid fraction containing soluble salts is recirculated to the absorber. The use of dual-alkali systems on utility boilers is attractive because of their ability to remove SO₂ very efficiently and to reduce scaling problems. The system has zero liquid discharge and eliminates the need for a waste water discharge permit. Using lime to capture the SO₂ reduces operating costs as compared to using either caustic or soda ash.

Dry and semi-dry scrubbing

There are four types of dry/semi-dry FGD - spray dryer absorber (SDA), sorbent injection, and dry circulating FGD. Both sorbent injection and spray dryer absorber processes are non-regenerative processes. The most common choice to date for dry scrubbing has been the spray dryer absorber, which is actually a semi-dry process. In this process atomized lime slurry is sprayed into the flue gas within the reaction vessel. SO₂ reacts with the atomized slurry to form calcium

sulphite (CaSO₃). A part of the CaSO₃ reacts with oxygen to form calcium sulphate (CaSO₄). The dried reacted particulates are collected at the downstream in an electrostatic precipitator or fabric filter. This process requires production of correctly sized lime slurry droplets and proper residence time such that the particulates are dry but well related when reaching the ESP or fabric filters. Although well-proven, this process can be difficult.

Sorbent Injection technologies require relatively low capital cost. A sorbent is injected into the boiler or flue gas Dry Injection type processes are available with lime, trona, activated carbon and other dry reagents. Such systems with more than 90% have been developed. The activity of sorbents are dependent on temperatures, e.g., activated carbon (<100°C), alumina- and silica-supported sorbents (300°C), alumina-CaO (120-240°C but regeneration with H₂ at 750-850°C). Since the flue gas temperatures in the burners range between 120°C to 250°C, SO₂ removal in this temperature is economical for industrial applications [14]. In circulating FGD solid lime and recirculated byproduct are injected together. Hydrated lime is injected directly in the CFB reactor. Water is injected independently. SO₂ removal efficiency of 93-97% can be achieved at a Ca/S molar ratio of 1.2-1.5. The process does not require any high maintenance mechanical equipment.

To address the issue of lower desulphurization efficiency of semi dry processes as compared to wet processes, powder particle spouted bed was developed [15]. Increasing the utilization of lime in semi-dry/dry FGD systems is one of the current challenges researchers have to deal with. Most of the approaches that have been applied to increase the performance of the sorbent make use of the capacity of the additive to increase the surface area of CaO. The reactivity of hydrated sorbents is closely related to the sorbent surface area. Inorganic hygroscopic salts such as barium, potassium, sodium and calcium chlorides and nitrates of sodium and calcium have been found to be effective in increasing the performance of hydrated lime. Some of the siliceous materials which are viable for conditioning of the hydrated material include fly ash, bottom ash and incinerator ash. Palm oil ash has also been used.

Selection of FGD Processes

Due to differences in site conditions, available resources, and waste stream requirements, SO₂ removal solutions are very site and process specific. Key design considerations to consider when selecting a scrubbing technology include inlet SO₂ concentration and variation, efficiency and outlet concentration requirements, scrubbing liquor pH, liquid-to-gas ratio, prevention of scaling and plugging, liquid and gas distribution and contact, by-product handling and disposal, remoteness of site etc. The regenerative FGD process is suitable for high concentrations of SO₂ such as copper converting units. The concentrated SO₂ stream from the regenerative methods can then be reduced to elemental sulphur with CH₄, H₂ or CO. The throw-away method is well suited for coal-based power plants with lower SO₂ concentrations (about 1000 ppm). Lime is the most important material used. About 70% of the FGD capacity in the United States use wet lime scrubbing with forced oxidation (LSFO), wet lime scrubbing with magnesium enhanced lime (MEL), or dry lime scrubbing using conventional spray dryer absorber. Dry lime scrubbing with circulating fluidized bed absorber is more widely used in Europe. Approximately 75% of the FGD systems installed on utility boilers are either lime or limestone scrubbing.

There have been significant improvements in the wet lime processes in recent years that have improved its performance and reliability, and reduced capital and operating costs. Such improvements include use

of a single absorber module for power generating units with (capacity 500 MW and greater and increase in sulphur dioxide removal efficiency (>95%).

The advantages of the wet scrubbing process are relatively high removal efficiency (90-95%), low cost of operation, minimal safety hazards (explosion, fires), and ability to collect both gas and particulate matters. However the disadvantages are wet waste production (contaminated scrubber liquid), formation of highly corrosive acids, and high power requirements. Waste water treatment is required in wet scrubbing systems. The waste stream produced contains sodium sulfite (for sodium based system), ammonium sulphite (for ammonia based systems) and gypsum (for limestone based systems). Although spray towers are most common, the Chiyoda and Alstom Flowpack immersion technologies and the Advatech Double Contact Flow Scrubber have gained some market share.

In terms of space requirement, the regenerative systems have little or no requirement for reagent preparation area. However, they require significant resources and space for solvent regeneration. Both regenerable and non regenerable systems can produce a saleable byproduct. However, since the markets for sodium sulphite or gypsum are limited, it is more common for the caustic, lime and limestone non regenerable systems to direct their byproducts to waste. On the other hand, the regenerable systems direct SO₂ into sulphuric acid or elemental sulphur markets. SO₂ can often be readily absorbed by the sulphur recovery units existing in most refineries, yielding elemental sulphur as a by-product.

Although the most common desulphurization methods are the "Wet" types, the total and the annual costs of the "Dry" ones are considerably less, due to simplicity, less water consumption and easier residues handling. The "Dry" methods are easily installed and require less space. Hence, they are good choices for the existing units modernization [16,17]. FGD can be classified as wet, semidry [15], dry process. Since the SO₂ recovery efficiency in "Dry" methods (50-60%) is considerably less than the "Wet" ones (93-98%), the dry methods are recommended in cases where SO₂ emission is low.

The scale of operation also influences selection of appropriate FGD technology. For example, the wet scrubber technology used in utility power plants is too large and costly for solid waste incinerators. On the other hand dry sorbent injection may be more suitable option for these applications due to low capital cost, small footprint, ease of operation, and flexibility to fuel changes. A new type of gas scrubber called the double-contact flow scrubber (DCFS) for flue gas desulphurization has been developed which achieved energy conservation together with high desulphurization and high dedusting efficiencies by spouting absorbent liquid from the new type of nozzles located at the bottom of the scrubber to ensure the better gas liquid contact [15].

The amount of energy consumed by an FGD process has a direct impact on the power plants heat rate and also on the available net electric generating capacity. The amount of sulphur to be removed depends upon the sulphur content of coal and the emissions control of the requirement. The following table gives an overall comparison of SO₂ control systems [18] Table 1, Figure 1.

Recovery of Sulphuric Acid

Various raw materials that can be used to manufacture sulphuric acid include elemental sulphur, sulphide ores, spent acid and gases like H₂S. When elemental sulphur is used, solid sulphur is melted and the liquefied sulphur is then purified and burnt to produce sulphur

System	Percent SO ₂ reduction	Capital cost (\$/kw)
Sorbent injection	30-70	50-100
Dry flue gas desulphurization	70-90	80-170
Wet flue gas desulphurization	>90	80-150

Table 1: Overall comparison of SO₂ control systems.

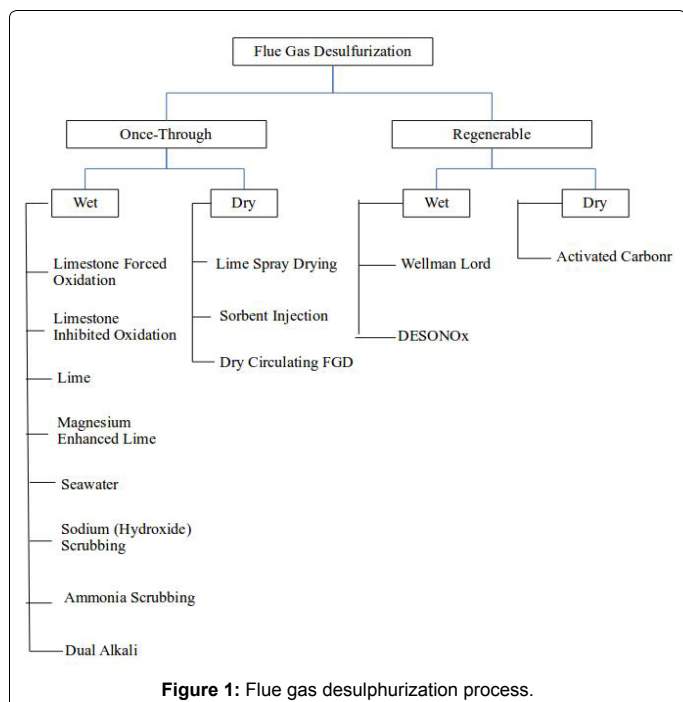


Figure 1: Flue gas desulfurization process.

dioxide. The gases are cooled and then passed through a multi-stage converter system. The conversion steps include (i) Conversion of SO₂ into SO₃ (ii) Absorption of SO₃ in H₂SO₄ for form H₂SO₄, with addition of appropriate amount of water to maintain the concentration of H₂SO₄ [19-22].

Regenerative SO₂ recovery systems are available, which are effective for variety of tail gases with varying SO₂ concentrations [23]. Processes for adsorption of SO₂ in activated carbon beds and periodical regeneration of the carbon with water washing to produce dilute H₂SO₄ of 15-20% concentration have been around since decades [24].

Production of sulphuric acid is considered to be the most viable option of sulphur recovery from smelter off gas and abatement of SO₂ emissions to the atmosphere. Thus processing of the SO₂ off-gas to sulphuric acid at pyrometallurgical smelters based on sulphidic ore concentrates of copper, nickel, lead or zinc, is a well-established process. In process development for metallurgical sulphuric acid plants a major objective has been to enable the operation with very high SO₂ concentrations, while simultaneously avoiding the generation of diluted gas.

Among the various FGD processes [25], the DeSONOX process produces sulphuric acid as the end product. Sulphuric acid can be produced in the Wellman-Lord Process by aqueous absorption and desorption, concentration and then oxidation of concentrated SO₂ to sulphuric acid catalytically [15,26].

The wet gas sulphuric acid (WSA) technology developed by Haldor Topsoe is a very popular and well accepted method to remove SO₂ and recover it in the form of concentrated sulphuric acid of commercial

grade. In a WSA plant, SO₂ conversion is similar to the SO₂ conversion in a conventional acid plant based on absorption, except the catalytic conversion takes place in a wet gas. The WSA technology treats the furnace off-gas directly from upstream gas cleaning plants. No further drying is required, since the humidity present in the off-gas is used to hydrate the SO₃ generated in the converter and produce sulphuric acid. More than 55 countries use the WSA technology developed by Halder Topsoe. Applications include refineries, coal gasification, metallurgical and mineral industry, power plant. The heat generated during the oxidation, hydration and condensation processes is principally reused in the process to preheat the off-gas to the required temperature level, and also to generate high pressure superheated steam for process use. This advantage of steam production, coupled with lower water and power consumption requirements, is particularly important in the African production environment. Having fewer process components than conventional acid plants, the WSA technology is a simple and compact operation, which makes it easier to retrofit into an existing smelter plant. Further, the WSA technology simultaneously offers the possibility to treat multiple gas streams arising within the production facility due to superior flexibility in terms of SO₂ concentration and turnaround ratio.

There are two main limitations of the WSA technology. The concentrations of SO₂ in the feed gas inlet should be restricted to 6-7% by volume. This is due to the need of restricting the dew points of sulphuric acid to around 260°C, from the consideration of the construction materials in the WSA condenser. Dilution of the gas with atmospheric air to overcome this limitation would increase the volume of the gas leading to the increase in the dimension of the plant. Secondly, since it is a single-contact process, the conversion is limited to typically 99.4 - 99.7%. Scrubbing of tail gas with caustic or hydrogen peroxide results higher conversion, but at the expense of additional investment and operating cost.

To address these issues, Topsoe has introduced the WSA-DC technology ("DC" means double condensation), that can accept feed gases with SO₂ concentrations of 13 volume% or higher. This technology is suitable only for applications where the water vapour content of the gas is controllable. H₂S gas with high water vapour content would result in production of acid of lower concentration.

The SNOx process is based on the WSA process and also includes integrated selective catalytic reduction DeNOx step. The SNOx process removes sulphur dioxide, nitrogen oxides and particulates from the flue gas, the sulphur is recovered as concentrated sulphuric acid and the nitrogen oxides are reduced to free nitrogen. The process involves catalytic reactions and does not consume water or absorbents [14,27]. Apart from the separated dust, no other waste is produced. Since this process can also handle other sulphurous streams, it is highly interesting in refineries. SNOx process increases thermal efficiency and reduces CO₂ emission when using high sulphur coal for power generation. The main advantages of this process are excellent heat recovery, reduced CO₂ emission, no process chemicals, no process water consumption, no production of waste solids and liquids, valuable sulphuric acid product, clean technology and low operating and maintenance cost.

MECS Sulfox technology is also a popular and well accepted technology to produce sulphuric acid from sulphur off gases. This is based on thermal and catalytic conversion of SO₂ into sulphuric acid. MECS also developed single stage HRS which also reduced the investment cost in heat recovery system installed in sulphuric acid plant. The benefits of this technology are no liquid effluent other than sulphuric acid (the product), very low acid mist emission, high

SO₂ conversion so low SO₂ emission, use of proven catalyst and low operating cost.

Emerging Trends

R&D efforts towards improvement of FGD technologies are directed towards addressing various issues that impact the cost, SO₂ absorption efficiency and energy consumption. Much of the research efforts on the limestone/gypsum process have been directed towards understanding the absorption process, which is a complex one due to the presence of soluble microparticles in the slurry [28]. Conventional wet limestone-gypsum FGD process has the problem of poor limestone utilization since limestone is not a very reactive reagent and does not completely dissolve in the scrubber system [Liu et al 2008]. Limestone is pulverized to an average size of 5 to 20 μ m (95% a 325 mesh) to improve its utilization, reduce FGD operating costs and solid-waste disposal volumes, and improve reliability as well as gypsum quality. However pulverization is associated with significant amount of power consumption and further increases the operation costs. Avoiding the requirement of additional power for pulverization has been a major focus for R&D efforts towards improvement of conventional wet limestone-gypsum FGD process. One of the approach for increasing absorption efficiency is the addition of amine. Reversible hydration and ionization reactions that take place for dissolved SO₂ in water solution and produce bisulphite and sulphite. Adding the amine, to the water increases the quantity of SO₂ dissolved as the amine drives the equilibria to the right by reacting with the hydrogen ions. Requirement of a large column packed with various packings or spray tower, rotating-stream tray scrubber, etc in the traditional SO₂ absorption process is responsible for high capital and operating costs. Improvement in mass transfer efficiency can reduce the size of columns. Process intensification can play an important role in this regard. In this context, rotating packed bed (RPB) has been studied [29]. It rotates a doughnut-shaped packing element to generate a centrifugal acceleration as high as several hundred folds of g to intensify mass transfer efficiency. Many gas-liquid contacting processes, such as distillation, absorption, extraction, desulphurization, deaeration, reactive precipitation, chemosynthesis, removal of dust, and making nano-material employ RPB.

To reduce the cost of flue gas purification, development of new technologies and equipments of simultaneous flue gas desulphurization and denitrification has become the leading research direction in the air pollution control field. In the recent years, the interests in simultaneous desulphurization and denitrification of flue gas increased rapidly. Many technologies have been proposed, among which the simultaneous removal of sulphur dioxide and nitrogen dioxide by using wet scrubber is most growing one.

Conclusion

Sulphur dioxide emission control is expected to assume more and more significance with the emission norms becoming even more stringent in future. At the same time SO₂ treatment methods need to have minimum waste disposal requirements, and also economical. Considering these, production of sulphuric acid is one of the best choice considering its economical values and utilities. The possibility of stricter regulations regarding GHG emissions in future may raise issues related to conventional wet scrubbing technologies in utilities. The limestone-sulphur dioxide reaction produces carbon-dioxide. On the other hand use of lime of mag-lime in wet scrubbers can be cost prohibitive [30,31]. The purpose of this study is to review the various methods of emission reduction of SO₂, the installation and operational cost as well as good environmental performance. Although many of the

processes for FGD are established since long, need for reducing cost, energy consumption and SO₂ removal efficiency are driving further R&D efforts. Various techniques for process intensification may play an important role towards development of better processes for SO₂ removal and generation of by-products like H₂SO₄.

References

1. Taieb D, Brahim AB, Chimie CR (2013) Electrochemical method for sulphur dioxide removal from flue gases: Application on sulphuric acid plant in Tunisia. C R Chim 16: 39-50.
2. Ravi K Srivastava (2000) Controlling SO₂ emissions: A review of technologies. US Environmental protection agency.
3. Wang G, Bing L, Yang Z, Zhang J (2014) Selective catalytic reduction of Sulphur dioxide by carbon monoxide over iron oxide supported on activated carbon, School of Chemical Engineering, Qingdao University of Science and Technology Qingdao China.
4. Taylor MR, Rubin ES, Hounshell DA (2005) Control of SO₂ emissions from power plants: A case of induced technological innovation in the U.S. Technol Forecast Soc Change 72: 697-718.
5. Bhanarkar AD, Rao PS, Gajghate DG, Nema P (2005) Inventory of SO₂, PM and toxic metals emissions from industrial sources in Greater Mumbai, India. Atmos Environ 39: 3851-3864.
6. Luvsan ME, Shie RH, Purevdorj T, Lkhagvasuren B, Barkhasragchaa B, et al. (2012) The influence of emission sources and meteorological conditions on SO₂ pollution in Mongolia. Atmos Environ 61: 542-549.
7. Darmastuti Z, Bur C, Möller P, Rahlin R, Lindqvist N, et al. (2014) SiC-FET based SO₂ sensor for power plant emission applications. Sens Actuators B Chem 194: 511-520.
8. Cofala J, Syri S (1998) Sulfur emissions, abatement technologies and related costs for Europe in the RAINS model database. International Institute for Applied Systems Analysis.
9. Dehghani A, Bridgman H (2010) Flue gas desulphurization methods to conserve the environment. Petroleum & Coal 52: 220-226.
10. Rameshni M, Santo S (2005) Production of elemental sulphur from SO₂ RSR. Resources and energy 1-19.
11. Wendt A (2002) Optimization of WSA technology, Masters Thesis, Lund University.
12. ZhongY, Gao X, Huo W, Luo Z, Ni M, et al. (2008) A model for performance optimization of wet flue gas desulphurization systems of power plants. Fuel Processing Technology 89: 1025-1032.
13. Evans AP (2009) Operational Experience of Commercial, Full Scale, Ammonia Based Wet FGD for Over a Decade. Environmental Technologies 1-19.
14. Ma JX, Fang M, Lau NT (1999) Simultaneous catalytic reduction of Sulphur dioxide and nitric oxide. Catal Today 62: 127-130.
15. Nakazato T, Yunyi L, Kunio K (2004) Removal of SO₂ in Semi-Dry Flue Gas Desulphurization Process with a Powder-Particle Spouted Bed. Can J Chem Eng 82: 110-115.
16. Weiss (1999) LH Evaluating sulphur producing FGD processes. Chem systems Inc.
17. Zhu T, Kundakovic L, Dreher A, Stephanopoulos M (1999) Redox chemistry over CeO₂-based catalysts: SO₂ reduction by CO or CH₄. Catal Today 50: 381-397.
18. Kataoka S (1992) Coal burning plant and emission control technologies, Technical Note World Bank China Country Department Washington DC.
19. Happel J, Leon AL, Hnato MA, Bajars L (1977) Catalyst composition optimization for the reduction of Sulphur dioxide by carbon monoxide. Ind Eng Chem Prod Res Dev 16: 150-154.
20. Wiltowski T (1995) catalytic reduction of SO₂ with methane over Molybdenum catalyst.
21. Paik SC, Kim H, Chung JS (1997) The catalytic reduction of SO₂ to elemental sulphur with H₂ or CO; Catalysis Today 38: 193-198.
22. Stephanopoulos MF, Zhu T, Li Y (2000) Ceria based catalysts for the recovery of elemental sulphur from SO₂ laden gas streams. Catal Today 62:145-158.

23. Puricelli S (2013) Regenerative SO₂ capture: recovering the future. Paper presented at Sulphur 2013, 29th international conference and exhibition, Miami, Florida, USA.
24. Ball Frank J, Torrence SL, Albert JR (1972) Dry Fluidized Activated Carbon Processes for Stack SO₂ Recovery as Sulfur. J Air Pollut Control Assoc 22: 20-26.
25. Buecker B, Hovey L (2012) Circulating Dry Scrubbers: A New Wave in FGD? Mid Atlantic Regional air management SO₂/HCl. control technology 115: 1-176.
26. Wang C, Lin S, Hwang W, Weng H (2002) Supported Transition-Metal Oxide Catalysts for Catalytic Reduction of SO₂ with CO as a Reducing Agent. Ind Eng Chem Res 41: 666-671.
27. Zhu Q (2010) Non-calcium desulphurisation Technologie. 42-44.
28. Liu Sy, Xiao d (2006) Modeling and Simulation of a Bubbling SO₂ Absorber with Granular Limestone Slurry and an Organic Acid Additive. Chemical Engineering and Technology 29: 1167-1173.
29. Xiuping J, Youzhi L, Meiduo GU (2011) Absorption of Sulphur Dioxide with Sodium Citrate Buffer Solution in a Rotating Packed Bed. Chin J Chem Eng 19: 687-692.
30. Asphahani AI, Nicholas AF, Silence WL, Meyer TH (1989) High performance alloys for solving severe corrosion problems in flue gas desulphurization systems. Materials and Corrosion 40: 409-417.
31. Kong Y, Davidson H (2010) Dry Sorbent Injection of Sodium Sorbents for SO₂, HCl and Mercury Mitigation. Proceedings of the 18th American Waste to Energy Conference NAWTEC18, Orlando, Florida, USA.

Citation: Roy P, Sardar A (2015) SO₂ Emission Control and Finding a Way Out to Produce Sulphuric Acid from Industrial SO₂ Emission. J Chem Eng Process Technol 6: 230. doi:[10.4172/2157-7048.1000230](https://doi.org/10.4172/2157-7048.1000230)