

**Research Article** 

# Life Cycle Assessment of the Environmental Impact of Biosurfactant Production from Oil Waste by a Diculture of *Azotobacter vinelandii* and *Pseudomonas* sp.

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#### Abstract

This study is aimed at carrying out a life cycle assessment of the environmental impact of biosurfactant production from oily waste by a diculture of Azotobacter vinelandii and Pseudomonas sp. The methodology used was the life cycle assessment according to the ISO 14-040 standard. The microorganisms used in the study were also isolated from the environment. The biosurfactant produced were quantified and the CO2 and NH3 that were produced were quantified also. The life cycle assessment as a gate - to - gate assessment was considered in this study. Two impact categories were selected for their relevance (global warming, and acidification/eutrophication potentials). The functional unit used for the impact analysis was based on the production of 1000 Kg of biosurfactant. The result showed that during the bioprocess of the biosurfactant production (by the diculture), the volume of CO<sub>2</sub> evolved was 28.23  $\pm$  5.08 cm<sup>3</sup>, which is equivalent to 0.056  $\pm$  0.01 g CO<sub>2</sub> per 100 ml of broth. In terms of g CO<sub>2</sub>/1000 Kg biosurfactant, 4545 ± 817.93 g CO<sub>2</sub> were Produced in this bioprocess. The life cycle impact assessment of biosurfactant production by this consortium, based on global warming potential was 0.046 tonnes/ 1000 Kg biosurfactant. Other impact values calculated for acidification and eutrophication potentials were 0.008 tonnes/1000 Kg and 0.0014 tonnes/1000 Kg of biosurfactant. In this work also, the consortium produced 1.22 ± 0.04 mg biosurfactant per 100 ml of cell - free broth. However, the individual organisms Pseudomonas sp. and Azotobacter vinelandii produced 1.03 ± 0.02 and 0.08 ± 0.001 mg of biosurfactants per 100 ml cell-free broth respectively. These values when compared with the individual organisms shows that using a consortium for the Bioprocess is more sustainable.

**Keywords:** LCA; Global warming potential; Acidification; Eutrophication potentials

# Introduction

Crude oil exploration and exploitation activities have resulted in inadvertent oil spill incidences. In Nigeria, increase in oil spill has been reported due to sabotage by the host communities in the Niger Delta region. Hence crude oil waste abounds in the Niger Delta areas of Nigeria. Oil wastes generated in the oil industries can be channeled into various biotechnologically tools. Environmental research is often technology dependent with new advances in thinking. Biotechnological conversion of the petroleum oily wastes into biosurfactant by a consortium of Azotobacter vinelandii and Pseudomonas sp is a welcome idea. In this work, we evaluated the environmental impact of biosurfactant production from oily waste by this consortium. The use of biosurfactants has gained ground due to the following advantages it possesses over the chemical surfactant. These include its biodegradability [1], low toxicity and availability of raw materials [2]. Biosurfactants also have some wide range of application in food and cosmetics industries and enhanced oil recovery and in bioremediation of the polluted ecosystem [3]. Due to these applications and demand, there is an increase in the use of microorganism in the production of biosurfactants.

The use microorganism in the production process of biosurfactants complies with the 12 principles of green chemistry. The principles include;

1. Prevention, 2. Atom Economy, 3. Less Hazardous Chemical Syntheses 4. Designing Safer Chemicals, 5. Safer Solvents and Auxiliaries, 6. Design for Energy Efficiency, 7. Use of Renewable Feedstocks, 8. Reduce Derivatives, 9. Catalysis, 10. Design for Degradation 11. Real-time analysis of Pollution Prevention and 12. Inherently Safer Chemistry for Accident Prevention [4,5].

Surfactants are amphiphilic molecules that accumulate at interfaces, decrease interfacial tensions and form aggregate structures such as micelles [6]. They normally possess both hydrophilic and hydrophobic moieties which confer the ability to accumulate in the oil and water interface. Biosurfactants on the other hand, are a structurally diverse group of surface-active substances produced by microorganisms. All biosurfactants are amphiphiles. They consist of two parts—a polar (hydrophilic) moiety and non-polar (hydrophobic) group that enables them to interact with the hydrophobic phase as well as the hydrophilic phase [7]. A hydrophilic group consists of mono-, oligo- or polysaccharides, peptides or proteins and a hydrophobic moiety usually contains saturated, unsaturated and hydroxylated fatty acids or fatty alcohols [8]. They are known to have surfactant activities which make them an interesting group of materials for application in many areas such as agriculture, pharmaceutical, cosmetic industries,

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waste utilization, and environmental pollution control such as degradation of hydrocarbons present in soil.

Biosurfactant are classified based on the nature of their polar groups. They are categorized mainly by their chemical structure and their microbial origin. In general, their structure which includes a hydrophilic moiety consisting of amino acids or peptides anions or cations; mono-, di-, or polysaccharides; and a hydrophobic moiety consisting of unsaturated, saturated, or hydroxylated fatty acids. The major classes of biosurfactants include glycolipids, lipopeptides and lipoproteins, phospholipids and fatty acids, polymeric surfactants, and particulate surfactants [9].

Biosurfactants have unique functional properties which drew much attention towards their use and applications. They have a broad range of functional properties. Most important is their environmental acceptability, because they are readily biodegradable and have lower toxicity than synthetic surfactants. The unique properties of biosurfactants allow their use and possible replacement of chemically synthesized surfactants in a great number of industrial operations. Moreover, they are ecologically safe and can be applied in bioremediation and wastewater treatment [10]. Some of the potential applications of biosurfactants include microbially-enhanced oil recovery, hydrocarbon degradation in soil environment and hexachlorocyclohexane degradation, and removal of heavy-metal from contaminated soil and hydrocarbons in aquatic environments [11].

Some microorganisms have the ability to utilize crude oil as a carbon source for biomass formation and energy. During this fermentation process, carbon iv oxide is produced and other processes in the product life cycle of the biosurfactant production have some environmental implications. To this end, it is necessary to assess the life cycle assessment of the production of biosurfactant in a view to find the areas of environmental hotspot. In this study, therefore, the environmental impact of producing biosurfactant from the consortium of Azotobacter vinelandii and Pseudomonas sp. was evaluated using Life Cycle Assessment (LCA) tools which is an analytical tool for the systematic evaluation of the environmental aspects of a product or service system through all stages of its life cycle. It is a methodological framework for determining and assessing the environmental impacts attributable to the life cycle of a product, such as climate change, stratospheric ozone depletion, eutrophication, acidification, toxicological stress on human health and ecosystems, the depletion of resources, water use, land use, and noise and others [12]. According to the Society for Environmental Toxicology and Chemistry (SETAC), LCA is defined as the: Process to evaluate the environmental burdens associated with a product, process or activity by identifying and quantifying energy and materials used and wastes released to the environment; to assess the impact of those energy and material uses and releases to the environment; and to identify and evaluate opportunities to affect environmental improvements [13]. Therefore, Life cycle assessment is a tool for assessing the environmental impacts of a product or product system over its entire life cycle. In a life cycle assessment (LCA), the different phases of a product's life cycle, like extraction of natural resources/raw material, production and manufacturing, distribution, use, maintenance, end-of-life treatment, recycling and final disposal, are included [14]. In this assessment, a Gate - to - Gate Life Cycle Assessment was considered.

Life cycle assessment (LCA) is necessary when assessing environmental impacts, in order to get the most precise idea of the environmental impact connected to a product or service delivered from a system [15]. By using LCA, issues of problem shifting can be revealed [15]. The problem shifting can be used in two ways: In the process of solving an environmental problem, the problem might either be shifted to another stage in the value chain or create a new environmental problem. This makes it crucial to have a consistent system description with clearly stated system boundaries. According to ISO 14040 [14]. Conducting LCA can be broken down into four main steps (Goal and scope definition, Inventory analysis, Impact assessment and Interpretation) as presented in the Figure 1.



Figure 1: The main steps of conducting an LCA [14].

# LCA Methodology

# Goal and scope definition

The goal and scope definition is the first thing that needs to be defined when conducting an LCA [16,17]. The goal of an LCA states the intended application, the reasons for carrying out the study and the intended audience for the assessment [14]. The goal and scope of this study is to determine the environmental implication of producing biosurfactant using *Azotobacter vinelandii* and *Pseudomonas* sp to determine which organism produces a more environmental impact. This study does not cover the whole product life cycle (cradle – to – grave) assessment, but rather, it covers a gate – to – gate assessment, where the assessment starts at some point in the technosphere but do not get to the end of life stage (disposal). The data generated will be used not just for academic purposes, but also for a comparism between other available data on biosurfactant. The processes with environmental hotspot will be identified while the type of impact will be identified and calculated.

# Functional unit and reference flow

An important part of the scope process is to decide the functional unit (FU) which provide a comparison basis. The functional unit describes the kind of function or service a product system delivers [18]. The primary purpose of a functional unit is to provide a reference to which the inputs and outputs are related [19]. The functional unit is a quantitative description of the service performance of the investigated product system [12]. Therefore, all of the environmental impact results from the LCA will be quantified relative to the functional unit, so the functional unit itself also has to be quantifiable. This makes it possible to compare results with other similar LCA studies with the same functional unit. The functional unit provides a reference to which the inputs and outputs are related [20]. This reference is necessary to ensure comparability of LCA results assessed on a common basis. Functional unit assesses the function performed by a product and indicates how much of this function is considered [21]. To be consistent with the surfactant manufacture processes, the functional unit of both surfactants manufactures was defined as the environmental performance per 1000 kg or per tonne of final biosurfactant. For example, the functional unit of CO<sub>2</sub> emission for this biosurfactant production is kg CO<sub>2</sub>/1000 kg Biosurfactant or tonne CO<sub>2</sub>/tonne Biosurfactant (t CO<sub>2</sub>/t Biosurfactant).

**Assumptions and limitations**: Since the full-scale manufacturing of the biosurfactant is still under development, a scaled-up production and application process will be proposed with a series of assumptions. To collect data for life cycle inventory, these assumptions provides important prerequisites to carry out calculations and estimations of the process data. Therefore, the LCA undertaken on the biosurfactant production process model is "from gate to gate" or partial rather than "from cradle to grave".

#### System boundaries

The system boundaries of a life cycle assessment study are defined by the inputs of raw materials, outputs of products and by-products, energy- and material flows that are involved in the process. System boundaries determine which processes are included (or excluded) in an LCA. Consequently, it is important to carefully consider where to draw the line between what should be included in the life cycle and what is insignificant for a given study [22-24]. Generally, system boundaries of LCA include the processes of raw material acquisition, recycle/disposal manufacturing, use/reuse/maintenance, and combined with the inputs and outputs related to the individual process (i.e., Raw materials, energy, emissions, wastes and releases). Disregarding the raw materials acquisition, energy extraction, product delivery, or application, the system boundary was restricted on the currently available simulated large-scale manufacturing process model.



It focused on the primary unit processes of manufacture and the proposed recycle utility of chloroform/ethanol, as shown below. In this system boundary, the gate-to-gate LCA analysis resources were inputs (raw materials and consumed energy) and outputs (emissions in air, water or solid wastes) associated with each life cycle stage of the manufacturing process (Figure 2).

#### Life cycle inventory

Upon completion of identifying the scope of the LCA, the next step is to conduct a life cycle inventory analysis (LCI), covering the data collection and calculation procedures [25]. Inventory analysis aims to quantify the inputs and outputs that cross the system boundary. The result of an inventory is a long list of material and energy requirements, products and co-products as well as waste and releases into air, soil and water. This list is referred to as the mass and energy balance or the inventory (Table 1) [26].

**Procedures for data collection:** To establish a life cycle inventory, the first phase is to survey and collect the life cycle data related to the product system, from inputs to outputs. In this case, the data collection was conducted on the entire Biosurfactant production process, as follows:

- Identify the inputs and outputs for each individual unit process for the industrial scale simulation of Biosurfactant production;
- Undertake mass and energy balance for the entire process;
- Quantify the amount of product, waste, material source and energy consumption;
- Convert the industrial scale data to the baseline of selected functional unit (mass per 1000 kg or tonne Biosurfactant).

**Biosurfactant production model and process assumptions:** Biosurfactants are produced as exogenous materials by microorganisms. During the breakdown of crude oil by organisms such as *Pseudomonas*, the produce exopolymeric substances that will help them to solubilize the crude oil. Therefore, in a media contain crude oil, these organisms can secrete surfactants which are harvested and used to improve remediation processes. There are also other uses of biosurfactant other than remediation. This process can be scaled up by using some software such as Super Pro Designer. The software is capable of handling material and energy balances, equipment sizing and costing, economic evaluation, environmental impact assessment, process scheduling and debottlenecking of batch and continuous processes [27].

Item	Quantity
Water	1000 ml
Crude oil	50 ml
MgSO <sub>4</sub> .7H <sub>2</sub> O	0.2 g
NaCl	0.1 g
(NH <sub>4</sub> )2SO <sub>4</sub>	0.1 g
FeCl <sub>3</sub>	0.02 g
Pseudomonas	0.5 × 10 <sup>7</sup> cell/ml
Chloroform	660 ml
Methanol	330 ml

Azotobacter vinelandii	0.5 × 10 <sup>7</sup> cell/ml
Sodium Benzoate	1.0 g
K <sub>2</sub> HPO <sub>4</sub>	0. 5 g
Mannitol	0.5 g
Ethanol	1.0 ml

 Table 1: Raw material for biosurfactant production in the laboratory scale and functional unit.

#### Life cycle impact assessment (LCIA)

Life cycle impact assessment (LCIA) is a phase where the results of the inventory are interpreted in terms of their impacts on the environment. LCIA provides the basis for analyzing the potential contributions of the resource extractions and waste/emissions in an inventory to a number of potential impacts. Raw material requirement is the sum of the net quantities (kg or tonne) of each raw material used within the process - subtraction between materials flowed in and out of the system:

#### Raw material requirement = $\Sigma_i$ Raw material used (Tonne)

Energy requirement is the sum of electricity consumption (the primary energy source based on the simulated process), which is converted to the energy requirement:

Energy requirement =  $\Sigma_i facto (MJkWh) \times electricity kWh$ 

#### Pollution potentials include

a) Global warming potential is a relative parameter which uses  $CO_2$  as a reference. The global warming potential of a given substance is defined as the extent to which a mass unit of the substance can absorb infrared radiation compared with a mass unit of  $CO_2$ . In this way atmospheric emissions can be converted to  $CO_2$  emissions with an equivalent greenhouse effect:

Greenhouse effect (GWP) =  $\Sigma_i GWPi \times emissions;$ to the air (Tonnes) [28]

For example, a process has 2.4 tonnes  $CO_2$  emissions and 1.5 tonnes  $CH_4$  emissions. The GWP factor for  $CO_2$  and  $CH_4$  is 1 tonne/tonne and 4 tonne/tonne, respectively. Thus, the GWP for this process= $2.4 \times 1+1.5 \times 4=8.4$  tonnes.

b) Nullification made by various forms of intervention in the environment can be determined by weighting with NP factors which are a measure of the capacity to form biomass, compared with phosphate Emissions to the atmosphere, water or soil (tonnes) is converted, using the NPi to an equivalent phosphate emissions (tonnes) in terms of eutrophication:

#### Nutrication (NP) = $\Sigma_i NPi \times emissions I$ (Tonnes)

For example, a process has 1.5 tonnes NH<sub>3</sub> emissions to the air. The NP factor for NH<sub>3</sub> (air or water) is 0.33 tonne/tonne. Thus, the NP for this process= $1.5 \times 0.33=0.495$  tonnes.

c) Acidification potential (AP) is the result of the release of nitrogen and sulfur oxides into the atmosphere, on soil and water that can vary the acidity in soil and water, with influences on both plants and fauna. It is measured with a reference to the effect of 1 kg SO<sub>2</sub>. Page 4 of 7

Acidification potential(AP) =  $\Sigma_i APi \times emissions i to the air +$ 

 $\Sigma_i AP \times emissions$  to water +  $\Sigma_i APi \times emissions$  i to the soil

For example, a process has 1.5 tonnes  $NH_3$  emissions to the air and 0.8 tonnes  $NH_3$  emissions to the water. The AP factor for  $NH_3$  (air) and  $NH_3$  (water) is both 1.88 tonne/tonne. Thus, the AP for this process= $(1.5+0.8) \times 1.88=4.324$  tonnes.

#### Life cycle interpretation

Life cycle interpretation occurs at every stage in an LCA. If two product alternatives are compared and one alternative shows higher consumption of each material and of energy and other impact indicators, an interpretation purely based on the LCIA can be conclusive [29]. In interpretation, a practitioner needs to analyze results, reach conclusions, explain the limitations and provide recommendations in accordance with the findings of previous phases of LCA, and to report the LCA results.

#### Statistical analysis

The analysis of variance was used to analysis the results using the statistical package for social science (SPSS v21). The result of the experiment will be presented as mean  $\pm$  standard deviation, while the significant differences in mean will be determined at  $p \le 0.05$ .

# Results

#### Studies of the microbial growth



**Figure 3:** Time-Growth curve of *Azotobacter vinelandii* and *Pseudomonas* sp. in their different basal media using glucose as a carbon source.

The result in Figure 3 above shows that the *Pseudomonas* sp has grown faster than the *Azotobacter vinelandii*. It also shows that the *Pseudomonas* sp has a lower generation time than the *Azotobacter vinelandii*. It reveals that the *Pseudomonas* sp attained maximum growth at about 12 hours while the *Azotobacter vinelandii* took about 60 hours to attain maximum growth.



**Figure 4:** Time - Growth curve of *Azotobacter vinelandii* and *Pseudomonas* sp. in their different basal media using crude oil as a carbon source.

Figure 4 reveals that *Pseudomonas* sp. and a consortium of *Pseudomonas* sp and *Azotobacter vinelandii* grow better in crude oil media when compared with the *Azotobacter vinelandii*. It also showed that the generation of time of the *Pseudomonas* sp. was lower than that of the consortium. While *Azotobacter vinelandii* did not show much growth in the media using crude oil as a carbon source.

#### Isolation of biosurfactants

Organism	Amount of Biosurfactants Produced (mg/100 ml) of cell free broth
Pseudomonas sp.	1.03 ± 0.03
A. vinelandii	0.08 ± 0.02
A consortium ( <i>Pseudomonas</i> sp. and <i>A. vinelandii</i> )	1.22 ± 0.03

 Table 2: Quantification of the Biosurfactants Produced by the organisms.

Table 2 shows that the consortium of the organisms produced the highest amount of Biosurfactant (1.22  $\pm$  0.03 mg/100 ml of cell free broth) when compared with the *Pseudomonas* sp. and the *Azotobacter vinelandii* while the amount produced by the *Azotobacter vinelandii* (0.08  $\pm$  0.02 mg/100 ml of cell free broth) was found to be the lowest of them all.

# Life cycle analysis

Determination of global warming potential (GWP) during the production of Biosurfactant.

The environmental impact of the biosurfactants was assessed by determining the global warming potential (GWP).

	Ps Media	Az Media	Ps+Az Media
CO <sub>2</sub> Released (cm <sup>3</sup> )	24.00 ± 4.33	3.56 ± 0.63	28.23 ± 5.08

Amount of CO <sub>2</sub> ( released	g)	0.047 ± 0.009	0.007 ± 0.001	0.056 ± 0.01
CO <sub>2</sub> (g)/1000 Kg Biosurfactant	of	4576.98 ± 825.13	8757.44 ± 555.06	4545.76 ± 817.93
Global warming potent (GWP) (tonnes/1000 I of Biosurfactant	ial kg	4.576 ± 0.825	8.757 ± 0.555	4.545 ± 0.8173

**Table 3:** The amount of  $CO_2$  emission given by producing 1000 Kg of Biosurfactant.

Table 3 reveal the global warming potential (GWP) for the production of 1000 Kg of Biosurfactant. *Pseudomonas* sp. gave a global warming potential of  $4.576 \pm 0.825$  tonnes/000 Kg of Biosurfactant, *Azotobacter vinelandii* alone gave  $8.757 \pm 1.555$  tonnes/1000 Kg of Biosurfactant and the consortium of both organisms gave  $4.545 \pm 0.817$  tonnes/1000 Kg of Biosurfactant produced.

# Determination of acidification potential (AP) during the production of biosurfactant

The environmental impact of the biosurfactants was assessed by determining the acidification potential (AP)

	Ps Media	Az Media	Ps+Az Media
$\rm NH_3$ Released (mg/100 cm <sup>3</sup> )	0.402 ± 0.09	0.521 ± 0.01	0.496 ± 0.02
NH <sub>3</sub> (Kg)/1000 Kg of Biosurfactant	0.39 ± 0.01	6.50 ± 0.01	0.41 ± 0.01
Acidification potential (AP) (tonnes/1000 kg of Biosurfactant	0.733	12.22	0.771

**Table 4:** the amount of emission given by producing 1000 Kg ofBiosurfactant.

The result in Table 4 showed the environmental impact of the biosurfactants assessed by determining the Acidification potential (AP). The AP showed that *Azotobacter vinelandii* produced the highest GWP while the consortium produced the least.

#### Electric Energy input during the production of biosurfactant

Equipment	Rating (W)	Time of used (hr)	Energy used (KJ)
Autoclave	750	0.25	0.1875
Waterbath	750	2	1.500
Refrigerator	250	24	6.000
Centrifuge	250	2	0.500
Oven	500	2	1.000
Total	2500	30.25	9.1875

**Table 5:** Electric Energy consumption during the biosurfactantproduction.

Table 5 showed that a total of 9.1875 KJ of Electric energy was used to produce 1.22 mg of Biosurfactant. Therefore, to produce 1000 Kg of Biosurfactant, a total of 7.531 GJ of Electricity will be consumed.

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# Total Emissions to the environment during the biosurfactant production process

EPA Emission factors of burning natural gas	Output to Nature
56 Kg CO <sub>2</sub> /GJ	1265.208 Kg CO <sub>2</sub>
44 g NOx/GJ	994.092 g NOx
19 g CO/GJ	429.267 g CO
4 g PM/GJ	90.372 g PM

Table 6: Evaluation of Output to the environment from burning of Natural gas. Keys: CO2=Carbon (IV) oxide; NOx=Nitrogen oxides; CO=Carbon (II) oxide; PM=Particulate Matter.

Table 6 showed the emissions to the environment which was calculated with the understanding that the Power transmission efficiency is at about 33%. Therefore the actual energy produced from natural gas will be 22.593 GJ. The result showed that about 1265 Kg CO2 will be introduced into the environment when 1.22 g of Biosurfactant is produced from the consortium.

# Discussion

The effect of crude oil pollution in Nigeria and its effect on the environment has been a major concern to the environmental scientist and the government at large. Methods of remediating polluted sites have been reviewed by many authors and the results have shown some level of successes. Out of the various methods of remediation, bioremediation has been proven to be the best method of remediation due to its environmentally friendliness and sustainability. One the microbial products used in the remediation of the environment is the Biosurfactant (a surface active compound). Biosurfactants on their own do not remove oily waste from the environment, but they have the potentials to lower the surface tension of these oily wastes (i.e., Emulsifying the oil) and to make them available for the indigenous organisms to degrade.

The result of the microbial growth using basal media for the organisms was determined and the result showed that the Pseudomonas sp grows faster when compared to the A. vinelandii. This is because A. vinelandii prefers mannose as carbon source and increase in biomass more than glucose probably that was why Mannose was used in the specific isolation of A. vinelandii. Also in the presence of high concentration of oxygen in the air, A. vinelandii uses more energy for protecting the enzyme (nitrogenase) and consequently produces a lower cell yield. It tends to consume more oxygen at the surface, thereby protecting the nitrogenase from inactivation by Oxygen. It can also increase the activities that may uncoupled respiratory electron transport system. In this process, the A. vinelandii uses the glucose more often to produce ATP and CO<sub>2</sub> instead of channeling it to biomass production. The ATP, thus produced is then channeled into nitrogenase protection. Thereby the growth of Azotobacter in the presence of oxygen is reduced. Pseudomonas on the other hand, uses oxygen and glucose. Though from the same genus as Azotobacter, Pseudomonas show no intolerance to glucose or oxygen. In using an in vivo expression technology (IVET), Redierset et al. screened a nitrogen-fixing Pseudomonas stutzeri strain for genes specifically expressed in rice rhizosphere. Sequence analysis of these genes revealed high sequence similarity not only to genes of several other

Pseudomonas strains but also to A. vinelandii genes. These observations and the availability of a genome sequence of A. vinelandii and several *Pseudomonas* species shows the phylogenetic relationship of A. vinelandii to Pseudomonas sensustricto. In practice, Pseudomonas can be used to create an anaerobic environment due to its ability to consume a lot of oxygen. Pseudomonas sp use glucose for ATP production and also for biomass production.

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The growth of the A. vinelandii, Pseudomonas sp. and a consortium of A. vinelandii and Pseudomonas species were determined in a mineral medium using crude oil as the sole carbon source. The result revealed that crude oil did not really support the growth of Azotobacter as the growth was very minimal when compared with the growth of Pseudomonas and a consortium of Pseudomonas and Azotobacter vinelandii (Figure 4). From the result, Pseudomonas sp was able to achieve maximum growth within 24 hours while the consortium was able to reach a maximum growth after about 48 hours. The exponential growth rate of the Pseudomonas sp. were found to higher with lower doubling time when compared with the Azotobacter vinelandii and the consortium. Some of the factors that can affect the generation time, which directly or indirectly affects generation include; environmental factors, availability of nutrient, temperature, pH and the size of the organism. From this result, one could suggest that crude oil is not a preferred nutrient source for A. vinelandii. But the Pseudomonas sp. grew well in the broth using the crude oil as a carbon source. After 24 hours, there was a decline in the microbial growth even when the crude oil has not been exhausted, suggesting that the crude oil being a mixture of organic and inorganic compounds containing some components which cannot easily be degraded by the organism. Some other reason could be that the Pseudomonas sp. has depleted some of the limiting nutrients such as nitrogen and phosphorus. In the consortium (A. vinelandii and Pseudomonas sp.), the microbial growth stained log phase of the microbial growth till about 48 hours suggesting that the interactions between the organisms which favor both organism.

The life cycle tools were used to access the environmental impact of producing 1000 Kg of biosurfactants. The Carbon iv oxide (CO<sub>2</sub>) produced by the organisms was used as a marker to determine the Global Warming Potential (GWP) of the production process. The result in Table 3 showed that *Pseudomonas* sp. produced 4576.9 ± 825.13 g of CO<sub>2</sub> during the production of 1000 Kg of biosurfactants. This amount to the GWP of  $4.576 \pm 0.83$  tons per 1000 Kg of biosurfactant. The Azotobacter vinelandii and the consortium gave  $8.757 \pm 1.568$  and  $4.545 \pm 0.82$  tons per 1000 Kg of biosurfactants respectively. The GWP follows this other Azotobacter vinelandii>Pseudomonas sp.>Azotobacter vinelandii and Pseudomonas sp.

Table 4 also showed the Acidification Potential (AP) of producing biosurfactant. The process of producing biosurfactant from Azotobacter vinelandii gave a high AP (12.22 tonnes/1000 Kg) of biosurfactant while the consortium gave 0.771 tonnes/1000 Kg of biosurfactant which is highly reduced when compared with Azotobacter.

The environment hotspot zone in the production of biosurfactant was assessed by determining the energy input in the form of electric energy use. In Table 5 the result showed that 9.1875 KJ of energy was consumed to produce 1.22 g of biosurfactant. Therefore, to produce 1000 Kg of biosurfactant, a total of 7.531 GJ of electricity will be consumed. According to the US power Agency, the national grid that supply electric energy from the combustion of natural gas is 33% efficient. In other words, total energy the plant need to supply is about 22.593 GJ of energy. According to the EPA, there are emission factors associated with burning of natural gas. The conversion factor show that 1265.21 KgCO<sub>2</sub>, 994.09 g NOx, 429.27 g CO and 90.37 g of particulate matter (PM) will be produced (Table 6). Using this LCA information, it will be noted that the transmission of power produced the highest environmental impact.

# Conclusion

The LCA shows that the process of producing biosurfactant did not show much impact on the environment. But the major environment hotspot was on the supply of power from natural gas. One would suggest that the purpose of producing the surfactant should be considered. If the purpose is for environmental bioremediation, it will be wise to apply the organisms directly to the soil. Since they can produce exopolymers with surfactant activities and also increase soil fertility. On the other hand, the use of hydroelectric power should be considered when it comes to the production of biosurfactant since the major pollution was coming from the supply of electricity.

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