

The Application of Transparent Glass Sponges for Improvement of Light Distribution in Photobioreactors

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Abstract

A new concept for improving light dilution and light distribution in photobioreactors by applying transparent, open-pored sponges was realized during cultivation experiments. A manufacturing process based on the polymer replica technique was established. A polyurethane template is impregnated with a nanoscaled SiO₂ powder suspension (solids loading of 60 wt% at around pH 10) and dried. The green body is prepared by burning-out the polymer at 800°C. Subsequently the sintering of the remaining SiO₂ structure to transparent cellular bodies is carried out at 1330°C. Many different factors influence the process. The slurry stabilization (viscosity, zeta-potential, pH) is important to generate a stable and self-supporting SiO₂ shell around the template and achieve appropriate green bodies. The sintering temperature determines the transition of amorphous (transparent) into crystalline silica. The 8 ppi sponge has a porosity of 0.9, the specific surface area of 568 m² means an increase of the (inner) surface to volume ratio of the reactor. Porous glass has a very high surface to volume ratio (about 0.26 m²/g of glass at 10 μm pore size). Because of multiple and complex reflection of light into the porous glass, the algae can obtain light energy at any location of the total volume. First cultivation experiments in special designed Miniplate reactors show an increase in growth rate (about +25%) at low cell densities. The photo conversion efficiency was enlarged from 4.9% for the empty reactor to 5.6% and 5.9% for the 8 and 15 ppi sponge filled reactor. The effect and the improved efficiency of biomass build-up per applied light will be more apparent at high cell densities. Therefore concentration of the standard Tris-Phosphate (TP) medium (2.5 fold) and feeding are necessary.

Keywords: Microalgae; Photo-bioreactor; Bioprocess design; Growth kinetics; Photo conversion efficiency; Light distribution; Light dilution; Transparent open-pored sponge

Abbreviations: CFD: Computational fluid dynamics; LM: Light microscopy; MRI: Magnetic resonance imaging; OD: Optical density; P_A: Areal productivity; P_V: Volumetric productivity; PAR: Photosynthetic active radiation; PCE: Photo conversion efficiency; ppi: Pores per inch; RMS: Root mean square; SEM: Scanning electron microscopy; SFR: Surface to footprint ratio; SVR: Surface to volume ratio; TAP: Tris Acetate Phosphate medium; TP: Tris Phosphate medium; XRD: X-ray diffraction; μ: Growth rate

Introduction

Decreasing oil resources force the interest in renewables for biofuel production as well as systems for production of raw materials in chemical industry and high-value products [1-4]. For this purpose phototrophic processes are advantageous using light as energy and carbon dioxide as carbon source for biomass formation with only little additional mineral nutrient necessary. Besides higher land plants like sugarcane, maize, canola and corn, algae show high potential because of higher growth rates and productivities as well as higher photosynthetic efficiencies (efficiency of biomass build-up from sunlight energy) [5-7].

Microalgae are aquatic unicellular and simple multicellular, microbial organisms. They perform no cell differentiation and the lack of additional supporting structures made of structural biopolymers like roots, stems and leaves in land-based plants enhances the photosynthetic efficiency [8]. When grown in photobioreactors cultivation is also possible in arid regions (possible land coverage) and not in competition with food production. Faster growth rates and more generation cycles during the year are advantageous. Furthermore the possible recycle of water and unconsumed nutrients and the tolerance to a high

CO₂ content in the gas phase which additionally increases growth kinetics make algae cultivations attractive compared to conventional agriculture.

Cultivation of microalgae in photobioreactors is state of the art and compared to open ponds highly controlled conditions can be applied (temperature, pH, aeration rate and CO₂ content, mixing, nutrients and additional feeding). However, not much large scale applications are in operation now, the few that exist produce high value products and no bulk materials e.g. for energetic use. Reasons for that are the high costs and the high demand of auxiliary energy e.g. for mixing. Although closed reactors are already better in light distribution compared to open ponds, there is still a need to reach the goal of reaching a homogeneous light distribution in the medium without the aforementioned disadvantages. Many different geometric modifications exist (e.g. flat plate or tubular reactors, airlift systems,...) all trying to overcome the problem of insufficient light supply for photosynthesis, but no optimal configuration has already been developed. The main problem of

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phototrophic processes is the demand of light as energy source which is not miscible as other substrates. Only low biomass concentrations are achievable due to the inadequate light supply of the whole culture. The light attenuation shows a very fast exponential decay above the layer thickness because of light absorption and scattering by the algae. Large volume elements offer only light limiting conditions resulting in no/less photosynthetic growth whereas on the illuminated surface light saturation or also photo inhibition occurs. So light dilution on the illuminated surface is one issue and diminishing the gradient in the bulk phase is another.

To date many different technical solutions have been described in literature all having the aim to improve light supply, e.g. horizontal and vertical tubular reactors in many different configurations or flat plate reactors with a small layer thickness also in special arrangements. Moreover specific configurations like the Flat Panel Airlift reactor (Subitec) or cheap low-ceiling designs made of plastic foils (Soilx and Proviron) [9-11] are proposed. All this configurations try to improve the surface to volume ratio (SVR) of the photobioreactor as well as the surface to footprint ratio (SFR). Both aspects intend to distribute the light over a larger reactor surface and avoid dark volume elements and to use the incident sunlight as efficient as possible (volumetric and areal productivity P_v and P_A). An optimization of the incident angle of sunlight hitting the reactor surface is a further option for possible developments [10-12].

The concept of this new approach is the enlargement of the inner surface area of the reactor which can contribute to illumination, light distribution and light supply. For this purpose transparent sponges made of glass are employed. In the investigation presented here they are placed in special designed Miniplate reactors for testing the effect. Maximum growth rates μ and the photo conversion efficiency (PCE) which means the efficiency of buildup of biomass from captured light are determined. Transparent glass sponges are a new class of materials. They are prepared by the polymer replica technique [13,14] employing polyurethane sponges with cell sizes of 8 and 15 pores per inch as templates and commercial available nanoscaled SiO_2 powders.

Necessary conditions for obtaining transparent open-celled glass sponges were presented in [13] where topics such as slurry stabilization, temperature for burning-out the polymer and subsequent sintering of the remaining SiO_2 structure to transparent cellular bodies are discussed. It was found, that concentrated suspensions at around pH 10 offer suitable properties for both, bringing enough particles onto the support for the formation of a stable and self-supporting SiO_2 shell and for successful sintering of the particulate framework to transparent bodies. Therefore, an adjusted burning-out process and an adequate sintering regime is necessary.

In order to obtain information about the developed phases as a function of sintering temperature-in particular the transition of amorphous into crystalline silica-X-Ray diffractometry was performed. Beside the stability and transparency of the manufactured open-celled sponges, for the successful use of the cellular material, the knowledge of its geometrical properties is necessary. In this study, these parameters are derived from calculations based on datasets of magnetic resonance imaging. Volume Image Analysis on the basis of magnetic resonance imaging (MRI) of porous media has been used now for several decades beginning with the aim of characterizing soil material, e. g. sandstones [15]. Increased resolution has enabled even a tomographic insight into such materials together with the possibility to analyze the structure with respect to geometrically characteristic parameters [16]. Its application to reticulated structures can therefore give the most extended

view into its details and has even been used recently to generate high resolution geometrical representations for computational fluid dynamics (CFD) calculations [17-19]. Additionally, scanning electron microscopy (SEM) and light microscopy (LM) were used for the characterization of the resulting transparent sponge structure.

Materials and Methods

Manufacturing and characterization of transparent sponges

Nanoscaled amorphous SiO_2 particles (AEROSIL OX50, SA of 50 m^2/g , Evonik Degussa GmbH, Essen, Germany) were dispersed in an aqueous media with a solids loading of 60 wt%. The pH of the slurries was adjusted at pH 10 employing 1 M tetramethylammonium hydroxide (TMAH, AlfaAesar, Karlsruhe, Germany). Details and characterization of suitable suspensions for the preparation of transparent sponges are described in [13].

As templates for the replica technique sponges (having 8 or 15 pores per inch (ppi), Foam Partner Fritz Nauer AG, Leverkusen, Germany) with dimensions 64 x 122 x 25 mm^3 , necessary to cover half of the reactor volume, were used. The polymeric sponges were dip-coated employing well-dispersed slurries and compressed while submerged in order to fill all the pores. The impregnated polyester support was then removed from the slurry and the excess material was squeezed from the foams by means of a rolling mill. The coated polymers were dried for 24 h at 40°C and 80% humidity. For burning-out the polymer, the coated preforms were placed in an alumina crucible and heated in a furnace (VMK 135, Linn High Therm GmbH, Eschenfelden, Germany) under an air flow rate of approximately 150 – 200 L/h. To allow the gradual decomposition and diffusion of the polymeric material, heating was performed carefully up to 800°C. Subsequently, the samples were sintered at air atmosphere in a chamber furnace (Nabertherm GmbH, Lilienthal, Germany) at 1330°C with heating rates of 30 K/min and a dwell time of 10 min.

Characterization: For the determination of phase composition after thermal treatments, X ray diffraction (XRD) spectra were recorded using a Siemens D500 diffractometer, operating with $\text{CuK}\alpha$ radiation at 40 kV and 25 mA. Macroscopic analysis was performed by image analysis using a digital camera integrated on an optical microscope (Olympus AX70, Pittsburgh, USA). In addition, volume image analysis was performed using magnetic resonance imaging (MRI). In the present work the ^1H -MRI measurements were taken on a BrukerAvance 200 SWB tomograph (magnetic flux density, 4.7 T; micro-2.5 gradient system generating up to 1 T/m). Therefore, the sintered transparent sponge samples were cut into pieces of 8 x 16 x 20 mm^3 and filled with an aqueous solution of copper sulfate (4×10^{-3} M) in order to accelerate the spin relaxation.

Volume imaging analysis of transparent foams: Starting point for the image analysis are the 3-d images of the sponges, consisting of gray values for the 256^3 voxels of the scan domain. Using this 3-d volume data of transparent sponge, a model of the solid surface could be extracted with digital filter routines for noise reduction and an individual threshold value to separate solid from void. The selected threshold directly influences the surface area and, thus, simply selecting a value is somewhat vague as this threshold additionally depends on the operational parameters when acquiring the raw data. In the present work an automatic selection procedure was used that is described in detail in [20]. The whole procedure was programmed using the freely available Visualisation Toolkit (VTK) [21]. The results of the procedure are discretized surfaces comprising typically 0.5 - 1 million connected tri-

angles with the exact number depending on the surface area and resolution. After discretization, calculating the surface areas can be done by a simple addition of these triangles areas.

In order to determine the porosity the void space on one side of the interface area can be filled with tetrahedral volume elements and again summed up to result in the volumes of the void phase. The tetrahedral meshes for this purpose were generated in this work using the commercially available meshing tool ANSYS ICEMCFD as this meshes can easily be imported by many simulation toolkits. In order to give an overview, in Figure 1 an image of the resulting geometry is shown.

Based on the detailed geometry of the samples an estimation of the extents of single pores has been derived. The proposed procedure starts with an estimation of points in the void phase that are assumed to be the pore centers. These points are determined by first calculating the Euclidean distance of every point in the void phase to the nearest surface point by application of the algorithm according to Saito and Toriwaki [22] and then searching local maxima in the 3-dimensional distance field. Twice of the local distance at these local maxima then gives an estimation of a minimal pore diameter. Using these values, a statistical analysis of the pore sizes was made. As a result, in Table 1 the average and the RMS values of the pore diameters as well as porosity and specific surface area for both 8 and 15 ppi glass sponges are given. Up to now, the influence of cell size of the foams on light distribution is not clear, but the structural parameters are intended to form the basic data for further analysis. These further studies are necessary, e.g. employing Monte-Carlo-Simulation of multiple light scattering, in order to correlate the parameters to the light distribution.

Cultivation in miniplate reactors

Strains and medium: *Chlamydomonas reinhardtii* wildtype wt13 [23] derived from the original Ebersold/Levine line 137c (CC-125 mt+) [24,25] was used as a model organism. For maintenance and preculturing the algae was continuously grown mixotrophic in liquid cultures of TAP media (Tris Acetate Phosphate) [26] under low light intensities ($50 \mu\text{E m}^{-2}\cdot\text{s}^{-1}$).

Miniplate reactors: Special Miniplate reactors were developed for testing the transparent glass sponges (Figure 2). These consist of stainless steel frameworks (bottom and top plate, two side plates) with the internal measurements of 140 x 100 x 20 mm and two glass panes bonded between the side plates using neutral crosslinking silicon rubber (SCRINTEC 600, RALICKS Industrie- und Umwelttechnik, Rees-Haldern, Germany). The bottom and top plate are sealed with a silicon gasket (1.5 mm VMQ-Elastomer, Angst + Pisterer, Zürich, Switzerland) and fixed with screws. For aeration and mixing a PTFE membrane (1 μm THOMAPOR-Poröse Platte, RTC ReicheltChemietechnik, Heidelberg, Germany) is fixed in the bottom plate. The inlet and

exhaust gas passes 0.2 μm sterilefilters, the connection to the plate is done via LUER-LOCK. For sampling a syringe is used connected to a safe flow valve (B.Braun, Melsungen, Germany) and a needle. Light is supplied using 60 LEDs (MS6L083AT, Nichia, Japan) with 6° collimating lenses (IMM Photonics GmbH, Unterschleißheim, Germany) in 100 mm distance from the illuminated side of the reactor.

Photoautotrophic cell growth was investigated in a working volume of 0.2 L 2.5xTP medium (TAP without Acetat), pH 8.8 at varying light intensities. Inoculation was done after saturation of the medium with CO_2 with a four days old preculture grown in TAP; the starting biomass was adjusted to approximately 0.05 g/L. The cell suspension was purged continuously with a sterile mixture of air enriched with 5% CO_2 at an aeration rate of 50 mL/min controlled via two mass flow controllers (MassFlo, MKS Instruments, München, Germany). Temperature was kept constant at 25°C via an incubator (Flohr Instruments, The Netherlands). Light intensity was controlled using the control system BioProCon written as a routine in Lab View (National Instruments).

The installation of the glass sponges into the Miniplate reactor is shown schematically in Figure 6. The microalgae cells are grown in suspension within the pores of the sponges. The separation of algae after cultivation is easily done. The liquid suspension is just draining off from the solid sponges and thereby the algae.

Analytcs and calculations:

- **Biomass determination:** Biomass concentrations were determined by offline optical density (OD) measurements at 750 nm using a spectrometer (T60 UV-Visible Spectrophotometer, PG instruments, Leicester, Great Britain).
- **Light measurements:** Measurements of light intensity were done using a planar quantum sensor (MQS-C, Walz connected with a LI-250 Light Meter, Licor, Walz Mess- und Regelungstechnik, Efeltrich, Germany). Light intensities up to 1500 $\mu\text{E}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$ were applied.
- **Calculation of specific growth rate:** The specific growth rate μ was determined in the exponential growth phase under non-light limiting conditions (dry biomass <0.2 g/L) according to the following formula.

$$\frac{dx}{dt} = \mu_{\max} \cdot x \quad (1)$$

with x biomass, t time and μ_{\max} maximum specific growth rate.

This can be converted to

$$x = x_0 \cdot e^{\mu_{\max} \cdot (t-t_0)} \quad (2)$$



Figure 1: Real (A) and reconstructed (B, C) structure from 1H NMR image of the polymer template transparent sponge and sintered at 1330°C.

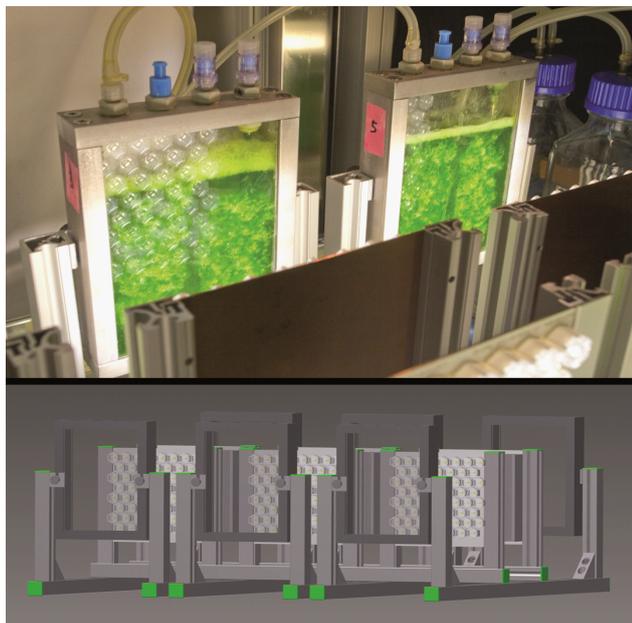


Figure 2: Mini-Plate Reactors as model system for testing transparent glass sponges.

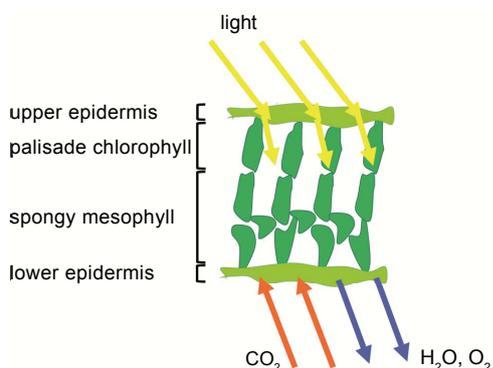


Figure 3: Schematic principle of leaf structure (leaf parenchyma) [10].

The values are averaged over at least three independent experiments.

- **Calculation of photo conversion efficiency (PCE):** The photo conversion efficiency (PCE) [J/J] describes the efficiency of biomass buildup from incident light energy. The following assumptions are used for calculation:

- biomass calorific value 20 MJ/kg [12,27]
- light energy conversion factor $1 \text{ W/m}^2 = 4.75 \cdot \mu\text{E}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$ (calculated from spectral distribution of used LEDs, for PAR photosynthetic active radiation 400-700 nm)

Finally a PCE based on PAR was calculated during the linear, light limited growth phase at higher cell densities (dry biomass <1 g/L) for defined light intensities. The values are also averaged over at least three independent experiments.

Results and Discussion

Anticipated effects of sponges for light dilution

The enlargement of the illuminated surface of photobioreactors is the main intention today to improve the efficiency of phototrophic cultivation systems. Data for SVR and SFR ratios of photobioreactors and open ponds are given in Table 2. “Natural photosynthetic systems” like trees could reach ten times higher values (Table 2). This can be explained by the “lime tree model” communicated by Pulz: the photosynthetic active leaf surface area accounts for 2500 m² and the footprint area for only 100 m². But comparing the illuminated surface area of photobioreactors with the leaf area of trees is only the first step for improvements.

The second step is based on an idea of nature inspired design published by Posten [10]. An additional effect on efficiency could be reached by enlargement of the inner surface of the reactor for light dilution and supply. Similar inner structures can be found in leaves of trees called the parenchyma (Figure 3). For this purpose transparent, open pored glass sponges are used as installations in photobioreactors. By inserting transparent 8 ppi sponges as light diluting materials into the reactor the SVR can be increased to a value of 568 m⁻¹ (see Table 1). An additional effect of the sponges would be the reduction of light gradients inside the whole reactor volume. Based on this concept photobioreactors still have quite promising potential for further developments.

The necessity of light dilution and the reduction of light gradients in photobioreactors can be explained with the growth kinetics of microalgae which show the growth rate depending on light intensity. Ex-

		8 ppi(glass)	15ppi(glass)
Porosity	-	0.90	0.86
Specific surface area	m ⁻¹	568	883
RMS pore diameter	mm	0.24	0.2073
average pore diameter	mm	3.56	2.79

Table 1: Foam parameters, obtained from volume analysis.

	Lime tree	PBR	Open Pond
SVR /m ² /m ³	<1000	<100	<4
SFR /m ² /m ²	<25	<10	1

Table 2: Values for surface to volume ratios (SVR) and surface to footprint ratios (SFR) for the lime tree model, photobioreactors and open ponds.

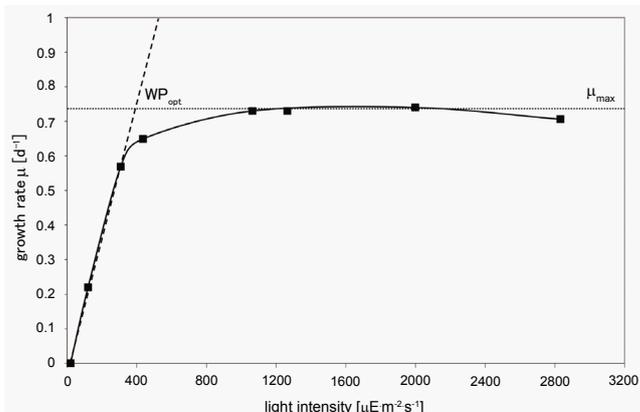


Figure 4: Growth kinetic of *Porphyridium purpureum* (modified based on [10]), with μ_{max} maximum growth rate and WP_{opt} optimal and most efficient working point of biomass production with highest increase of growth with rising light intensity.

empharilly the growth kinetic of the red algae *Porphyridium purpureum* is displayed in Figure 4. The different effects of light intensity on microalgal growth can be observed from this data. Growth is light limited at low light intensities up to about $400 \mu\text{E}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$. Then the optimal and most efficient working point of biomass production is reached with highest increase of growth with rising light intensity. At light intensities $>400 \mu\text{E}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$ photosynthesis becomes light saturated and later even inhibited. That means the more light energy supplied to the cultures cannot be stored in biomass or products.

The low efficiencies of production systems today is the combined effect of different light conditions outside and inside the reactors on growth increased even due to the change of optical densities of the algae suspension during the cultivation process. Figure 5 depicts schematically conditions in plate reactors illuminated from one side at changing cell densities. Only at low cell concentrations when all algae obtain sufficient light for growth the maximum growth rate μ_{max} will be reached. With increasing optical density of the suspension volume elements with light limited conditions (μ_{lim}) or even no cell growth ($\mu=0$) will exist. The overall growth rate measured under this condition will be a combination of all these effects.

For optimization of light dilution in photobioreactors transparent open pored sponges could be used as installations (for a schema see Figure 6). The algae grow in suspension within the pores of the sponge. The sponge structure dilutes light into the deeper, dark parts of the reactor by light conduction in the struts, as well as reflection and refraction at the surfaces due to the refractive index of glass which is higher than those of water. Therefore an amorphous SiO_2 glass structure has to be produced. Ideally sun light should be diluted to the optimal light intensity in the whole cultivation volume. Thereby the efficiency of production scale reactors could be improved by maximizing overall growth rates.

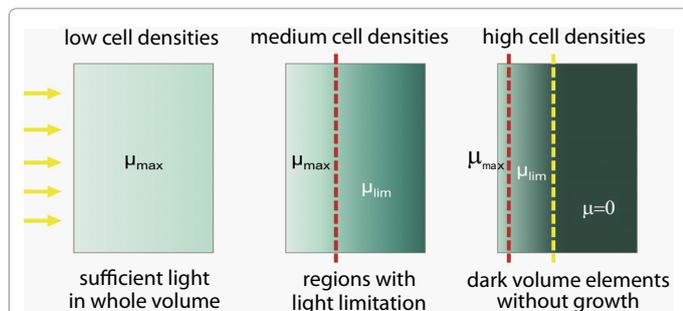


Figure 5: Schema of light conditions in a plate photobioreactor illuminated from one side at different cell densities, with μ_{max} maximum growth rate, μ_{lim} light limited growth rate, $\mu=0$ no cell growth.

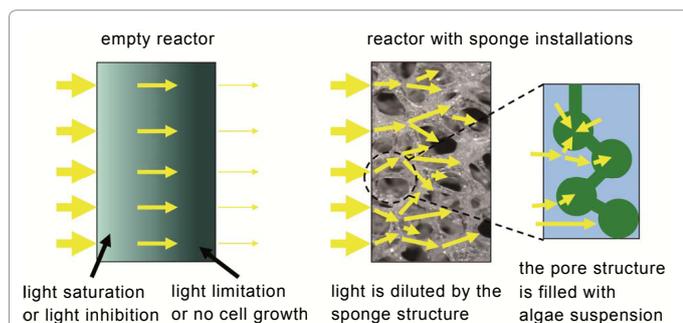


Figure 6: Installation of glass sponges into Mini-Plate Reactors, Schema of light dilution.

Preparation and characterization of transparent open-pored structures

Suspension: stability and viscosity: In order to identify a suitable pH-range for electrostatic stabilization of the silica particles ζ -potential measurements were performed [13]. Low-viscosity slurries are necessary for coating the polymer. In the system SiO_2 - water a compromise between a maximum of ζ - potential and suitable viscosity was obtained at a pH level higher than pH 10.

Using well stabilized slurries, an increase of SiO_2 leads to a moderate increase of viscosity and therefore a maximal concentration with acceptable viscosity values was obtained for slurries with solids loadings up to $\Phi < 60 \text{ wt}\%$.

Coated, dryer and burning out the polymer template: The aim of the impregnation process is to achieve a coating layer of defined thickness on the polymer template, consisting of dense and homogeneously packed SiO_2 nanoparticles. Both, structure and thickness of the layer depend strongly on the suspension used. The dominating parameters which control these factors are the solids loading, the interparticle forces and as consequence the viscosity. With respect to a sufficient coating layer thickness, a high solids loading is desirable. A dense and homogeneous particle packing requires repulsive interparticle forces. Both can be achieved by adjusting the pH-value as discussed previously.

Burning out the polymer is a very important step for obtaining manageable green bodies. A special temperature regimen has to be applied and a sufficient concentration of SiO_2 on the struts is necessary to prevent the framework from collapsing. Therefore, the solids loading of the slurry should be high.

Regardless the used slurry, the recommended amount of SiO_2 should be higher than approximately 0.1 grams per cubic centimeter of template. Below this value for the polymer employed in this study [8 and 15 ppi] it was not possible to get the desired structure through the burning-out process [28]. But if the thermal treatment is successful, there is no significant change in structure visible to the naked eye and the color of the samples remain white.

Figure 7 depicts a coated sample before (A) and after burning out the polymeric framework (B). It is worth to note, that the geometrical density of the shown greenbody was $>0.1 \text{ g/cm}^3$. In the case of a density of 0.08 g/cm^3 , see Figure 8, the framework was pulverized during the burning-out step.

Sintering and characterization: After the burning-out step, the obtained green bodies can be densified by viscous-flow sintering, leading to shrinkage of about 20% in all directions. By carefully selecting the sintering regime, i.e. an appropriate heating rate, temperature and dwell time, the initial white green bodies can be transferred into transparent open-celled foams. Transparency indicates that the amorphous character of the initial powder is still present. To monitor the phase composition XRD spectra were performed after sintering at temperatures varying from 1150 to 1400°C . In Figure 9, typical XRD-diffraction patterns of amorphous SiO_2 after sintering at 1350°C are shown. Above this temperature, SiO_2 foams commence to crystallize, as indicated in the XRD- spectra (Figure 9). Hence, after sintering at 1400°C the XRD pattern corresponds to crystalline cristobalite as the only detectable phase.

The broad peak near 22° is attributed to the short-range order in amorphous silica, whereas the sharp peaks in Figure 9 (right side) show the formed crystalline structure of cristobalite.

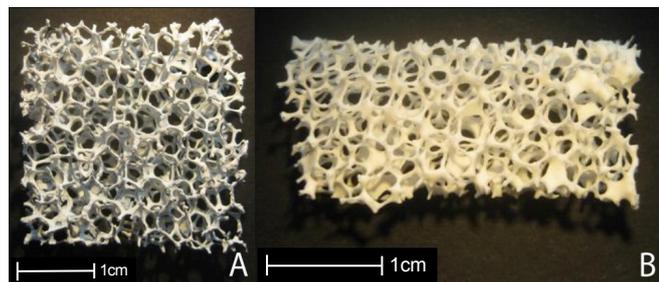


Figure 7: Coated sample before (A) and after burning out the polymeric framework (B), geometrical density of the greenbody >0.1 g/cm³.



Figure 8: Pulverization of the framework during the burning-out step, geometrical density of the greenbody 0.08 g/cm³.

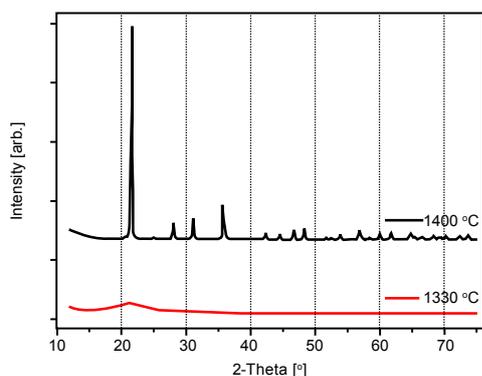


Figure 9: Typical XRD-diffraction patterns of amorphous SiO₂ after sintering at 1350°C.

Additionally to the XRD spectra, changes in structure and consequently on the transparency can be explained considering the apparent density and SEM analysis. These topics were extensively discussed in our previous work [28].

Cultivation experiments/ Determination of growth rates and photo conversion efficiencies (PCE)

The aim of experiments performed in Miniplate reactors is to test the transparent glass sponges as light diluting and light distributing installations in photobioreactors. Relevant parameters to estimate in this context are the growth rate μ in the exponential growth phase at

low cell densities and non-limiting conditions and more important the photo conversion efficiency (PCE) at high cell densities. The latter is a measure for the efficiency of biomass buildup from the captured light energy.

The reference system is the “empty” reactor applied for growth experiments without any light distributing installations inside. To increase the final cell densities reached in the reactor already concentrated medium (2.5xTP) is used at the beginning of the cultivation with CO₂ supply by aeration (5%). Typical growth curves of batch experiments at a selected light intensity (500 $\mu\text{E}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$) and the corresponding light transmission behind the reactor for 8 and 15 ppi glass sponges and the empty reactor are shown in Figure 10.

A characteristic growth curve of micro algal batch cultures is observed with a very short exponential phase until day one at low cell densities <1 g/L. Already at day one light becomes limiting but in contrast to other substrates it constantly further supplied which results in a transition into a linear growth phase. When Ammonium is limiting in the medium (ionchromatography measurements not shown) the maximum biomass concentration of about 3-3.5 g/L is reached during the third day.

The light transmission on the non-illuminated side of the reactor decreases in correlation with the increasing biomass concentrations resulting in light limiting conditions with transmission equals zero at day one. The light transmission at the beginning of the cultivation is lower with sponge filled reactors compared to the empty one. This is possibly due to a better light distribution inside the reactor caused by refraction and scattering. It could be a first indication for a better light dilution in the reactor by the sponge structure. It is also possible that by scattering at the sponge surface some amount of light is lost at the top, bottom and the small dark sides of the reactor. This amount is potentially bigger than in the empty reactor but could not be measured. The portion of scattering due to cells would be equal in all three systems. The measured reflection at the illuminated surface is less than <10% of the incident light intensity and no difference between the different configurations (empty or sponge filled reactor) can be observed. The influence of reflection at the reactor surface (typically 4% for air-glass) on incident light energy is eliminated by calibrating inside the reactor

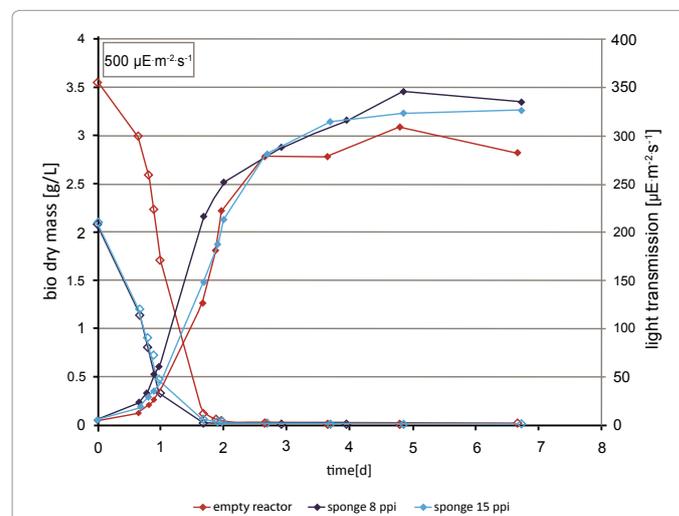


Figure 10: Bio dry mass concentration of wt13 and light transmission over cultivation time for 8 and 15 ppi glass sponges and the empty reactor 500 $\mu\text{E}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$, 2.5xTP, 5% CO₂ supply by aeration.

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